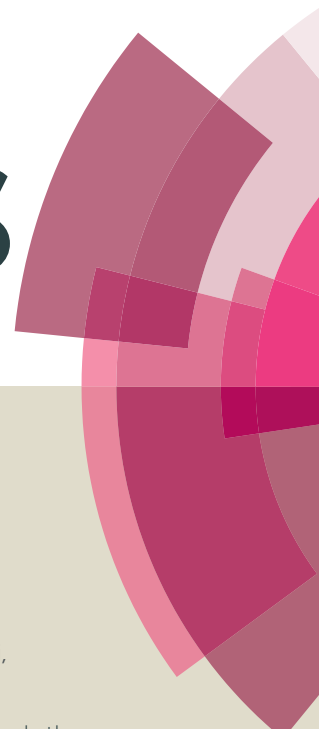


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Morphology-dependent Properties of CeO₂ Nano-catalysts on CH₂Cl₂ Oxidation

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Four types of CeO₂ nanoparticles with different morphologies (nanorods, nanocubes, nanopolyhedra, and bulk CeO₂ nanoparticles) were synthesized and used in dichloromethane (DCM) oxidation. Their detailed physicochemical properties were investigated by X-ray diffraction, N₂ physisorption, H₂ temperature-programmed reduction, high-resolution transmission electron microscopy, and X-ray photoelectron spectroscopy. Results indicated that DCM oxidation over CeO₂ nanoparticles has significant morphology-dependent effects. CeO₂ nanorods showed the best activity among all the investigated samples (T₉₀ is only 323 °C). The main products were CO₂ and HCl, although trace amounts of CHCl₃, CCl₄, CO, and Cl₂ could be detected. The high performance of CeO₂ nanorods in DCM oxidation may be related to the abundant surface defects, increased amount of adsorbed active oxygen species, and good reducibility of the catalyst.

1 Introduction

The chlorinated volatile organic compounds (CVOCs) emitted by numerous industries are highly toxic, carcinogenic, and genotoxic to humans, even at very low concentrations [1]. Thus, various countries set stringent emission ceilings to these harmful compounds. In addition, several abatement techniques have been developed to meet the increasingly strict legislations. Catalytic combustion is one of the most promising approaches to destroy CVOCs because it can be operated at a relatively low temperature range as compared with the thermal incineration process [2]. The formation of NO_x can also be restrained.

Undoubtedly, the catalyst is a key factor in CVOC oxidation. A suitable catalyst is highly active for the target CVOCs and should have good selectivity for the desired products (CO₂ and HCl). Supported noble metals [3-5], transition metal oxides [2, 6], and zeolites [7, 8] are usually reported in CVOC oxidation. Supported noble metal catalysts show relatively higher activity than the other two counterparts in a low-temperature range but are easily poisoned by chlorinated intermediates from CVOC destruction [9, 10]. Although the transition metal oxides are less active than the supported noble metals in most cases, these catalysts are believed to be more resistant to chlorine poisoning [2, 11]. Notably, transition metal oxides are also more abundant and much cheaper than noble metals. Therefore, the use of transition metal oxides to substitute noble metals in CVOCs oxidation is highly significant. However, their activity in the low-temperature range still needs to be

resolved.

CeO₂-based catalysts have been extensively studied in CVOC oxidation for their unique redox properties and high C–Cl bond dissociation ability [2, 12-15]. However, the strong adsorption of chloride species on the surface of CeO₂ during CVOC destruction will cause the partial deactivation of the catalysts [12, 15]. A conventional approach to resolve this problem is to incorporate CeO₂ with other transition metal oxides [2, 13-15]. However, deactivation could be still observed. Recently, CeO₂ nanoparticles with anisotropic shapes at the nanometer scale have attracted much interest. These materials can significantly improve the reaction performance when their specific facets are selectively exposed [16-19]. The morphology effects of ceria nanoparticles have been identified in CO [20-22] oxidation and the WGS reaction [23, 24]. However, the morphology-dependent properties of CeO₂ in CVOC oxidation have not been fully studied, although this oxide is widely used as catalyst in CVOC destruction. Herein, three types of low-dimensional CeO₂ nanoparticles (nanorods, nanocubes, and nanopolyhedra) were synthesized by a facile hydrothermal method and used in dichloromethane (DCM) oxidation. This study aimed to explore the structure–activity relationship of CeO₂ nano-catalysts during DCM oxidation.

2 Experimental

2.1 Catalyst preparation

Cerium (III) nitrate hexahydrate (Ce(NO₃)₃·6H₂O), sodium hydroxide (NaOH), and DCM were analytical grade reagents. All chemicals were purchased from Aladin Reagents and used as received without further purification. The synthesis of CeO₂ nanorods and nanocubes followed the revised procedure of Mai et al [25]. Typically, Ce(NO₃)₃·6H₂O (3.4720 g) and NaOH (33.6 g) were dissolved in 20 mL and 140 mL of deionized water, respectively. The two solutions were subsequently mixed in a Teflon bottle, and the mixed solution was stirred for 30 min at room temperature to form a slurry. The Teflon bottle

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was tightly sealed and placed in a stainless-steel autoclave. The tightly sealed autoclave was hydrothermally treated at 100 °C for 24 h. After cooling, the obtained white precipitates were collected by centrifugation, washed with deionized water for 3–4 times, and dried at 60 °C in air overnight. The acquired yellow powder was calcined in air at 450 °C for 5 h in a muffle furnace to obtain the CeO₂ nanorods. The synthesis of CeO₂ nanocubes was similar to that of CeO₂ nanorods, except the hydrothermal treatment temperature was set to 180 °C. The synthesis of CeO₂ nanopolyhedra mainly followed the procedure of Si et al [24], but the calcination temperature was revised to 450 °C. Typically, Ce(NO₃)₃·6H₂O (3.2567 g) was dissolved in 150 mL of NaOH solution (0.1 M). The mixture was stirred for 10 min at room temperature and transferred into a Teflon-lined stainless-steel autoclave. The autoclave was tightly sealed and hydrothermally treated at 180 °C for 24 h. The subsequent steps were followed to produce CeO₂ nanorods. For comparison, bulk CeO₂ nanoparticles were also prepared by directly calcinating Ce(NO₃)₃·6H₂O in air at 450 °C for 5 h. For convenience, the CeO₂ nanorods, nanocubes, nanopolyhedra, and bulk nanoparticles were denoted as CeO₂-r, CeO₂-c, CeO₂-p, and CeO₂-b, respectively.

2.2 Catalyst characterization

Powder X-ray diffraction patterns (XRD) were obtained on an X'Pert Pro powder diffractometer with the scanning rate of 0.1° per minute, using Cu K α radiation ($\lambda = 0.154056$ nm). The phase compositions were analyzed using jade 6.5.

N₂-physical adsorption and desorption were recorded on Micromeritics ASAP 2020 at 77 K. The specific surface area of the samples was calculated from adsorption isotherms using the BET equation.

H₂ temperature-programmed reduction (H₂-TPR) was measured on FINE SORB-3010 E instrument equipped with a thermal conductivity detector (TCD). 200 mg of sample was heated from 50 to 900 °C in a 10 vol% H₂/Ar flow (30 mL min⁻¹) at a ramp of 10 °C/min.

High Resolution Transmission Electron Microscope (HR-TEM) images of the samples were obtained using Philips-FEI (Tecnai G2 F30 S-Twin). All samples were ultrasonically dispersed in absolute alcohol for 1 h, then the suspension was deposited on an amorphous carbon-coated circular copper grid before measurement.

X-ray photoelectron spectroscopy (XPS) spectra of the samples were recorded on a Kratos AXIS Ultra DLD photoelectron spectrometer (Shimadzu scientific instruments, Japan) and using a monochromatic radiation source Al K (45 W, 3×10⁻⁹ mbar). The charging of samples was corrected by setting the binding energy (BE) of adventitious carbon (C 1s) at 284.8 eV.

Laser Raman spectra were obtained on LabRAM HR-800 spectrometer (Horiba Jobin Yvon, France) equipped with an air-cooled multichannel CCD detector, Ar⁺ ion (531.95) was employed as an excitation source (Nd: YAG 20 mW) to obtain visible Raman spectra.

2.3 Activity test

DCM oxidation experiments were conducted in a fixed bed tubular reactor (6 mm i.d.) under atmosphere pressure between 150 °C and 450 °C. 200 mg catalysts (40-60 mesh) was loaded in the center of the reactor and sandwiched with quartz wool. 1.8 g of quartz sand was placed on the inlet-end to preheat the feed gas. DCM feed concentration was kept constant at 1000 ppm by controlling the flow rate of bubbling air (20.8% O₂ and 79.2% N₂) through an ice bathed saturator, and the gas hourly space velocity (GHSV) in the reactor bed was set to 15000 mL g⁻¹ h⁻¹ by adjusting the flow rate of balance air in all experiments. The effluent gases were analyzed online with a GC-1620 gas chromatograph equipped with a flame ionization detector (FID) and a TCD. A further detailed analytic process was described in our previous work [6].

3 Results and discussion

3.1 Catalytic activity results

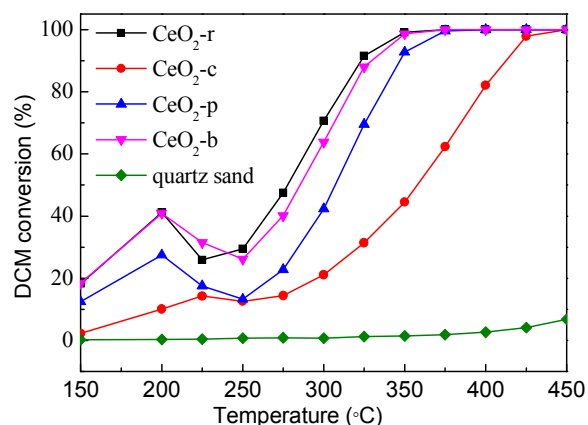


Fig. 1 Light-off curves of DCM over CeO₂ with different morphologies (1000 ppm DCM, air balance, GHSV: 15000 mL · g_{cat}⁻¹ · h⁻¹)

Fig. 1 shows the DCM conversion over CeO₂ nanoparticles with different morphologies. The pure quartz sand had almost no catalytic activity under the given testing conditions. The complete conversion of DCM could be achieved at 350–450 °C for all investigated samples. The values of T₅₀ and T₉₀ (temperatures with 50% and 90% DCM conversion achieved, respectively) are listed in Table 1. At T₉₀, the activity of the investigated samples was CeO₂-r > CeO₂-b > CeO₂-p > CeO₂-c. The CeO₂ nanorods showed the best activity; its T₅₀ and T₉₀ were only 278 and 323 °C, respectively. By contrast, the CeO₂ nanocubes showed the worst activity. Compared with the CeO₂ nanorods, the T₅₀ and T₉₀ of CeO₂ nanocubes increased 81 and 90 °C, respectively. DCM oxidation showed the different activities of CeO₂ nanoparticles with different morphologies.

Fig. 1 also shows that DCM conversion experienced temporary deactivation in the temperature range of 200–250 °C, which could be attributed to the chlorine species adsorption on the catalyst's active sites in relative low temperature range during DCM destruction. Similar phenomena were also observed by Dai et al

[26]. However, the gradual removal of Cl adsorption on the oxygen vacancies would be done thanks to the elevated temperature and high ratio of O/Cl in the feed gas [11]. Consequently, the activity of ceria was gradually recovered as the temperature increased.

The desired products of DCM oxidation are CO₂ and HCl. However, the poor selectivity may produce more toxic by-products. The main products of DCM oxidation over the investigated samples are CO₂ and HCl, with a small amount of trichloromethane (TCM), carbon tetrachloride (CCl₄), CO, and Cl₂, depending on the catalysts used.

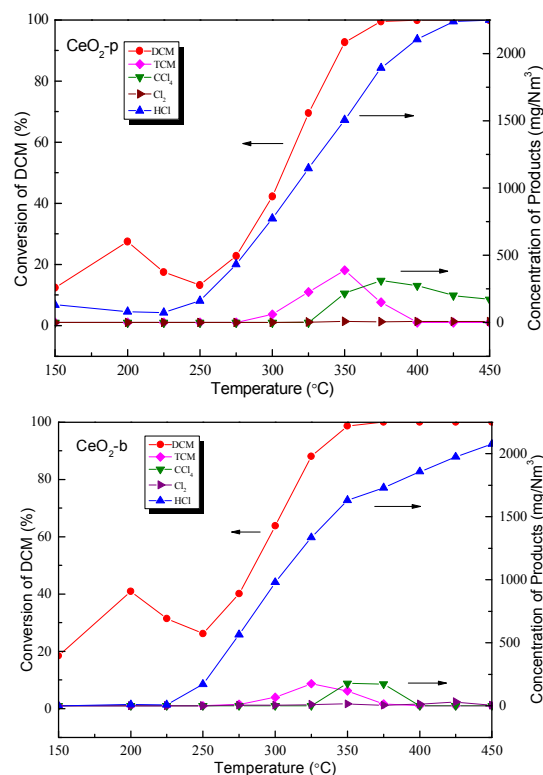
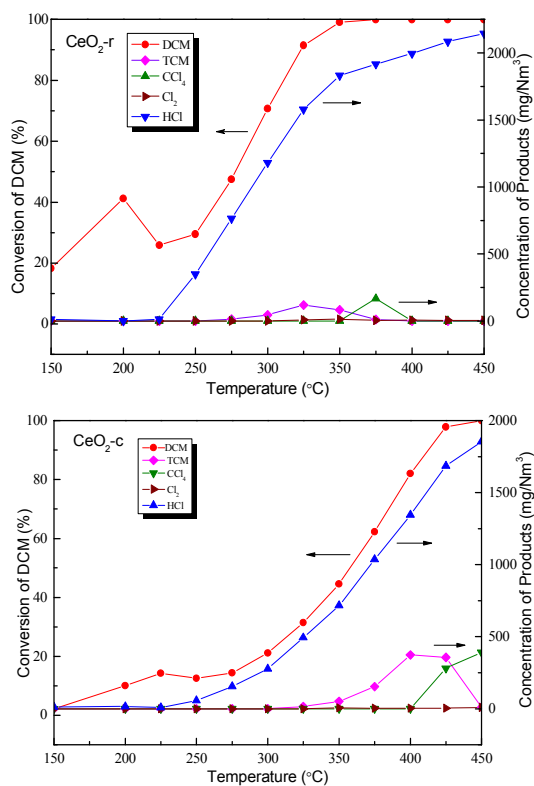


Fig. 2 Selectivity of chlorinated species during DCM oxidation over CeO₂ with different morphologies (1000 ppm DCM, air balance, GHSV: 15000 mL · g_{cat}⁻¹ · h⁻¹)

Fig. 2 shows the selectivity of chlorinated species during DCM destruction. The maximum selectivity of HCl over CeO₂-r, CeO₂-c, CeO₂-p, and CeO₂-b was 65.46%, 56.61%, 72.56%, and 66.22%, respectively. For TCM, the order of maximum selectivity was CeO₂-p (350 °C) > CeO₂-c (400 °C) > CeO₂-b (350 °C) > CeO₂-r (325 °C). (Henceforth, the numbers in brackets indicate the corresponding temperature.) For CCl₄, the order of maximum selectivity was CeO₂-p (375 °C) > CeO₂-c (425 °C) > CeO₂-b (350 °C) > CeO₂-r (375 °C). CeO₂-r showed the worst selectivity for TCM and CCl₄ with the maximum concentrations of 118 and 116 mg/Nm³, respectively; its selectivity was much less than when CeO₂-p was used as a catalyst (the maximum selectivity of TCM and CCl₄ was 374 and 390 mg/Nm³, respectively). Meanwhile, a small amount of Cl₂ was also detected on all the investigated samples in the high-temperature range (above 300 °C), which could be related to the Deacon reaction (2HCl + 1/2O₂ = H₂O + Cl₂) [26, 27].

Table 1 Textual properties and activity data of the investigated samples

Samples	Crystallite Sizes ①/nm	BET area /m ² g ⁻¹	Total pore volume /cm ³ g ⁻¹	Pore sizes /nm	T ₅₀ /T ₉₀ /°C	H ₂ consumption ^② /μmol g ⁻¹	I _D /I _{F2g}
CeO ₂ -r	10.3	86.4	0.33	15.3	278/323	722	0.058
CeO ₂ -c	40.9	20.5	0.15	29.3	359/413	74	0.023
CeO ₂ -p	12.9	68.0	0.10	6.1	308/346	413	0.033
CeO ₂ -b	12.9	67.6	0.23	13.8	286/331	495	0.036

① The value were estimated by Scherrer equation, applied to the (1 1 1) reflection of CeO₂.

② The values were calculated from the reduction of standard CuO.

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3.2 X-ray diffraction

The X-ray diffraction patterns of as-prepared samples are shown in Fig. 3, and the corresponding crystallite sizes are listed in Table 1. The diffraction peaks in 28.5°, 33.1°, 56.3°, and 59.1° can be clearly observed on all testing samples, which could be indexed to the cubic fluorite CeO₂ crystal phase (PDF# 89-8436, space group: Fm-3m). The diffraction peaks of CeO₂-c were much narrower than those of other samples, which was consistent with the larger crystallite sizes of this sample, as listed in Table 1. The results were also consistent with those of high-resolution transmission electron microscopy (HR-TEM) characterization (see below).

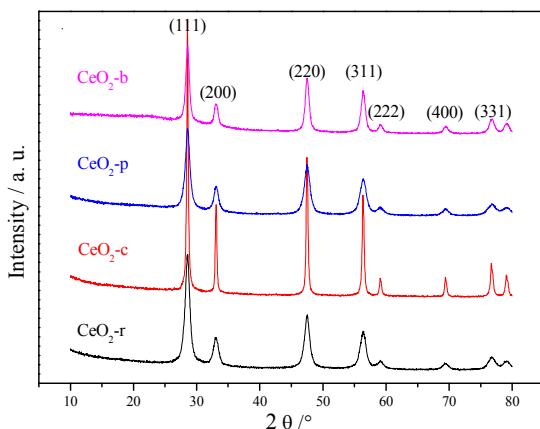


Fig. 3 The XRD patterns of investigated samples

3.3 N₂ physisorption by the Brunauer–Emmett–Teller method

The Brunauer–Emmett–Teller (BET) areas and corresponding pore volume and pore sizes of the investigated samples are listed in Table 1. CeO₂-r and CeO₂-c have the largest and smallest BET area as well as the best and worst activity during DCM oxidation, respectively. However, the activity of CeO₂-p was much inferior to that of CeO₂-b, although their BET areas were relatively comparable. These discrepancies could be also observed between the pore volume, pore sizes, and their activity in DCM oxidation. Therefore, the BET areas, pore volume, and pore sizes of nano-CeO₂ are not key factors of DCM oxidation. Other reasons may influence the activities of CeO₂ nanoparticles with different morphologies.

3.4 H₂ temperature-programmed reduction

The H₂ temperature-programmed reduction (H₂-TPR) of investigated samples is shown in Fig. 4. All tested samples displayed two or more reduction peaks involved different positions and relative intensities in the temperature range of 50–900 °C. Three main reduction peaks could be identified in the temperature range of 300–450 °C (α), 450–700 °C (β), and >700 °C (γ), respectively. The low-temperature reduction peak α involved a stepwise surface reduction process with the formation of nonstoichiometric CeO_{2-x} phase and oxygen vacancies in the

surface layer [28]. These reduced oxygen species are usually attributed to the chemical adsorbed oxygen on the vacancies of CeO₂ [22]. For peak β , characterized with some connected reduction peaks, usually involved the reduction of subsurface layer and deep interior of CeO₂ nanoparticles [28]. The more complex reduction profiles of CeO₂-c, CeO₂-p and CeO₂-b indicate some kind of structural inhomogeneities of these samples as revealed in the next TEM characterizations. The peak γ at the high-temperature range (ca. 800 °C) is attributed to the reduction of bulk lattice oxygen anions of CeO₂ [12, 29]. It should be mentioned that the initial reduction temperature of capping oxygen ions was changed with the testing samples: CeO₂-r (145 °C) < CeO₂-b (154 °C) < CeO₂-p (168 °C) < CeO₂-c (173 °C), thereby indicating that the morphologies of CeO₂ influenced the activity of capping oxygen. The H₂ consumption of the investigated samples in the low-temperature range was calculated; the results are listed in Table 1. The order of H₂ consumption was CeO₂-r > CeO₂-b > CeO₂-p > CeO₂-c, which is mainly consistent with their activity in DCM oxidation (Fig. 1).

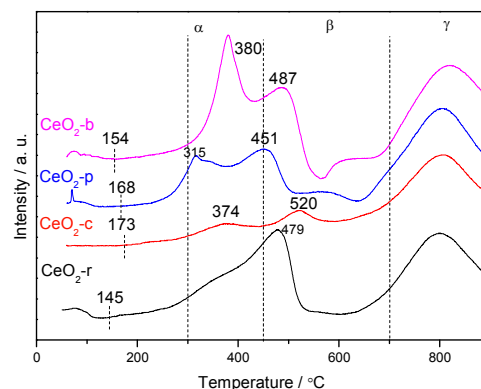


Fig. 4 H₂-TPR of investigated samples

3.5 HR-TEM

HR-TEM micrographs of the as-prepared samples are shown in Fig. 5. The morphologies of nanorods, nanocubes, and nanopolyhedra can be clearly observed, which are consistent with the experimental designs. The CeO₂-b nanoparticles were severely aggregated but no specific shapes were exhibited. Fig. 5a shows that the CeO₂ nanorods have a diameter distribution of 6–7 nm and a length distribution of 40–65 nm; their surfaces are rich in micropores. Fast Fourier-transform (FFT) revealed that the growth of CeO₂ nanorods are oriented in the [1 1 0] direction to expose the {1 1 0} and {1 1 1} planes (Fig. 5b). The CeO₂ nanocubes had a less uniform size distribution, with side lengths ranging from 50 nm to 100 nm, but all were cubic in shape (Fig. 5c). FFT revealed that this sample had selectively exposed {1 0 0} and {1 1 0} planes (Fig. 5d). The CeO₂ nanopolyhedra had a size distribution of 10–12 nm and selectively exposed {1 1 1} planes (Figs. 5e and 5f, respectively). Similar results were reported in [17, 24, 25]. Micrographs showed that the CeO₂ nanocubes had the

largest sizes, which is consistent with their having the smallest BET area and narrowest XRD peaks, as revealed in Table 1 and Fig. 3, respectively.

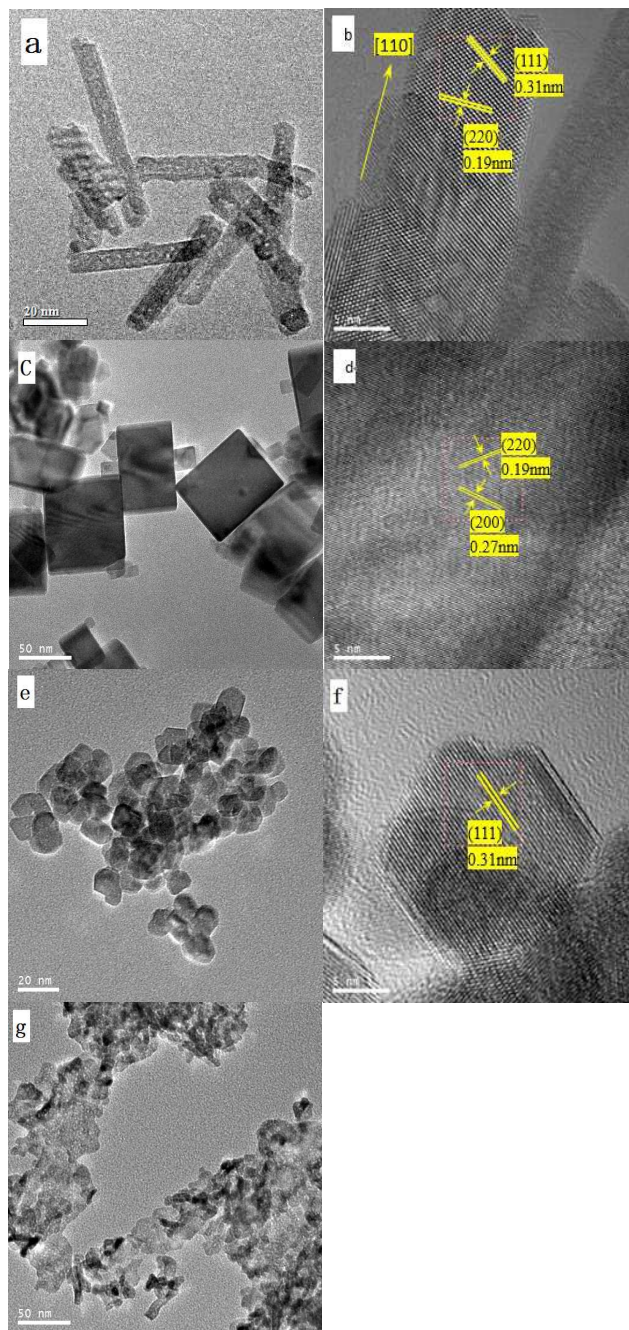


Fig. 5 HR-TEM of nano-CeO₂ with different morphologies (a, b: CeO₂-r; c, d: CeO₂-c; e, f: CeO₂-p; g: CeO₂-b)

3.5 X-ray photoelectron spectroscopy

The Ce 3d and O 1s X-ray photoelectron spectroscopy spectra of the as-prepared samples are given in Fig. 6(a). The six characteristic bands of Ce⁴⁺ can be clearly identified. The BE states of u''' (916.9 ± 0.1 eV) and v''' (898.3 ± 0.1 eV) are the result of the Ce 3d⁹4f⁰ O 2p⁶ final state. The lowest BE states of u'', v'', u, and v are located at 907.3, 888.5, 901.3, and 882.7 ± 0.1 eV; these states

are results of Ce 3d⁹4f¹ O 2p⁵ and Ce 3d⁹4f² O 2p⁴ [30]. No obvious bands corresponding to the Ce³⁺ states could be indexed, thereby indicating that the surfaces were almost complete oxidized over all the investigated samples or that the amount of Ce³⁺ is very low but similar in the four types of ceria [31]. By the deconvolution method, the O 1s core level peak in CeO₂ could be indexed to three bands. The BE in 529.3–529.5 eV could be assigned to lattice oxygen (O_{latt}) [15, 32], whereas the BE in 531.0–531.4 eV is ascribed to surface-adsorbed oxygen (O_{ads}) [15, 32, 33]. The high BE in 533.0–533.5 eV is attributed to the surface hydroxyl species and/or adsorbed water [32–34]. The ratios of each surface oxygen species were calculated, and the results are listed in Table 2. This table shows that the amount of oxygen species was significantly different for all investigated samples. The order of adsorbed oxygen species was CeO₂-r > CeO₂-b > CeO₂-p > CeO₂-c. Surface adsorbed oxygen species are known to have high mobility and usually regarded as active oxygen species in CVOC combustion [33, 35, 36]. This could explain the high performance of CeO₂-r in DCM oxidation. The activity of the investigated samples was basically consistent with the amount of adsorbed oxygen species on their surface (Fig. 1).

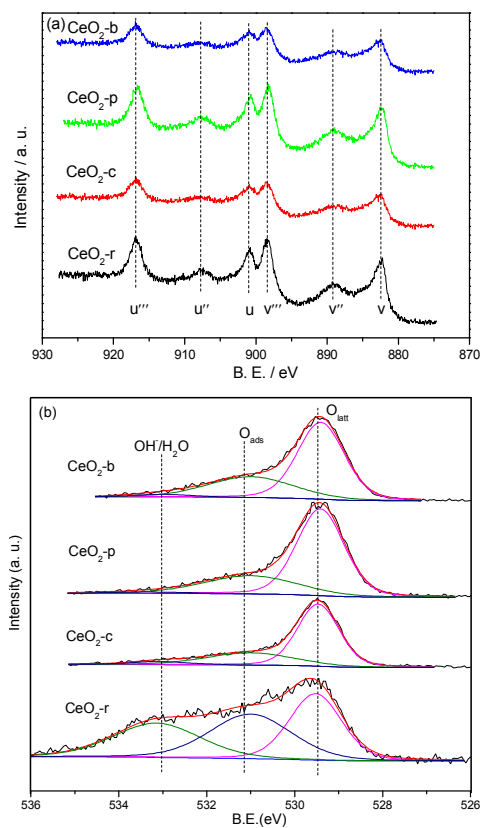


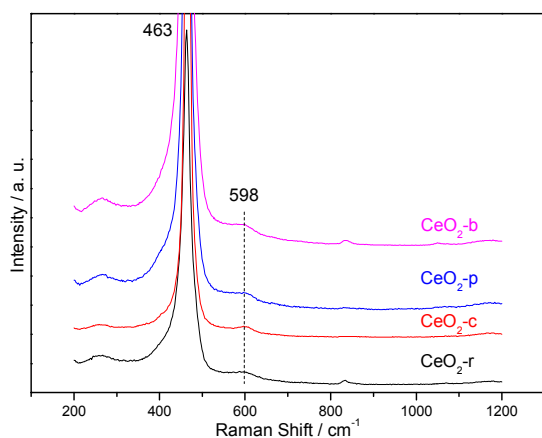
Fig. 6 XPS profiles of CeO₂ with different morphologies: Ce 3d (a) and O 1s (b).

Table 2 Amount of each surface oxygen species

Samples	Lattice oxygen		Adsorbed oxygen		OH ⁻ and/or H ₂ O	
	%	BE (eV)	%	BE (eV)	%	BE (eV)
CeO ₂ -r	34.3	529.5	36.1	531.0	29.7	533.1
CeO ₂ -c	67.3	529.5	28.0	531.0	4.7	533.1
CeO ₂ -p	69.3	529.4	28.9	531.0	1.8	533.3
CeO ₂ -b	65.1	529.4	32.2	531.0	2.7	533.0

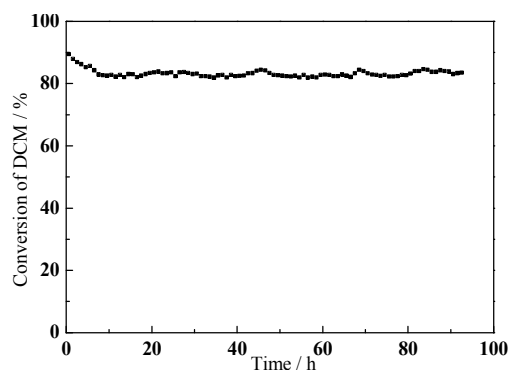
3.6 Raman spectroscopy results

Raman spectroscopy, known to be highly sensitive for detecting the concentrations of the oxygen vacancies of CeO₂, was performed here for CeO₂ with anisotropic shapes. As shown in Fig. 7, a strong band in about 463 cm⁻¹ and a weak band in about 598 cm⁻¹ were clearly observed on all samples, which could be indexed to the F_{2g} and defect-induced (D) models of cubic CeO₂ fluorite phase [20, 31], respectively. Also the relative intensity ratio of I_D (598 cm⁻¹)/I_{F_{2g}} (463 cm⁻¹) was used to estimate the defect concentration on CeO₂, and results were listed in Table 1. The I_D/I_{F_{2g}} ratio of all tested samples followed the order CeO₂-r > CeO₂-b > CeO₂-p > CeO₂-c, indicating that the CeO₂-r have more defect concentrations than the others. The results were also consistent with their activity in DCM oxidation.

**Fig. 7** Raman spectra of CeO₂ with different morphologies

4 Stability test of CeO₂ nanorods in DCM oxidation

Since CeO₂-r was highly active in DCM oxidation among all investigated samples, the stability of this sample in DCM oxidation was investigated in 325 °C for 100 h continuous testing, the result is shown in Fig. 8. It could be observed that CeO₂-r experienced a slowly deactivation in the initial 7 h testing, then stabilized. The conversion of DCM could be maintained at 83%–85% hereafter. The initial deactivation of CeO₂-r could be attributed to the adsorption of chlorine species on the surface of CeO₂ as discussed above.

**Fig. 8** Stability test of CeO₂-r in DCM oxidation at 325 °C (1000 ppm DCM, air balance, GHSV: 15000 mL · g_{cat}⁻¹ · h⁻¹)

5 Discussion

CeO₂ nanorods, nanocubes, and nanopolyhedra were well synthesized by a facile hydrothermal method. Using DCM oxidation as a model reaction, the morphology-dependent properties of CeO₂ nano-catalysts were investigated. CeO₂ nanorods showed much higher activity and better selectivity than CeO₂ nanocubes, CeO₂ nanopolyhedra and bulk CeO₂ nanoparticles in DCM oxidation. XRD results showed that the four synthesized samples exhibited cubic fluorite CeO₂ crystallite phase with different crystallite sizes. No other crystallite phases can be identified. The discrepancies of the tested activity with their crystallite sizes, BET surface areas, total pore volume, and pore sizes imply that the morphologies properties of ceria may play important roles in DCM oxidation. H₂-TPR results showed the reducibility and H₂ consumption of CeO₂ followed the order: CeO₂-r > CeO₂-b > CeO₂-p > CeO₂-c, which is mainly consistent with their activity in DCM oxidation. HR-TEM showed that CeO₂ nanorods selectively exposed {1 1 0} and {1 1 1} planes, CeO₂ nanocubes selectively exposed {1 0 0}, {1 1 0} planes, and CeO₂ nanopolyhedra selectively exposed {1 1 1} planes, while the bulk CeO₂ nanoparticles presented undifferentiated shapes. It is well known that the CeO₂ {1 1 0} planes and {1 1 1} planes are both nonpolar surfaces composed with stoichiometric Ce⁴⁺ and O atoms, while the {1 0 0} surfaces of CeO₂ are polar planes with O atom layers terminated [20]. The nonpolar {1 1 0} and {1 1 1} surfaces may benefit the adsorption of DCM with nonpolar properties. Given the deconvolution of O 1s core level spectra, the amount of adsorbed oxygen species on the surface of CeO₂ followed the order: CeO₂-r > CeO₂-b > CeO₂-p > CeO₂-c. It is generally accepted that the adsorbed oxygen species are active in CVOC destruction; thus, the activity of ceria with anisotropic shapes was mainly consistent with the order of their adsorbed oxygen species. Generally, the adsorbed oxygen species are usually related to oxygen vacancies on the surface of CeO₂. Raman spectra showed the defect concentration on CeO₂ also followed the order: CeO₂-r > CeO₂-b > CeO₂-p > CeO₂-c. Since the {1 1 0} surfaces are more exposed Ce cations than the {1 0 0} and {1 1 1} surfaces, the electrostatic interactions between the adsorbed oxygen species and Ce cations are stronger on CeO₂ nanorods than on CeO₂ nanocubes and CeO₂ nanopolyhedra; thus, it is rational that the stability and amount of adsorbed oxygen species on the CeO₂ {1 1 0} plane are more than those on the {1 0 0} and {1 1 1}

planes. The results are also consistent with the order of oxygen vacancy formation energy of CeO₂ surfaces: {1 1 0} < {1 0 0} < {1 1 1}, as demonstrated by DFT calculations [20, 24, 31]. Therefore, CeO₂ nanorods showed better performance in DCM destruction than the CeO₂ nanocubes, CeO₂ nanopolyhedra, even bulk CeO₂ nanoparticles.

6 Conclusions

CeO₂ nanorods, nanocubes, and nanopolyhedra and bulk CeO₂ nanoparticles were well synthesized and used in DCM destruction. Characterization revealed that CeO₂ nanorods selectively exposed {1 1 0} and {1 1 1} planes with better reducibility, as well as more surface adsorbed oxygen species and oxygen vacancies concentration than the other samples. Therefore, CeO₂ nanorods showed the best activity and good stability during long-term testing in DCM oxidation.

Acknowledgement

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Notes and references

- [1] S. Ojala, S. Pitkaaho, T. Laitinen, N.N. Koivikko, R. Brahmi, J. Gaalova, L. Matejova, A. Kucherov, S. Paivarinta, C. Hirschmann, T. Nevanpera, M. Riihimaki, M. Pirila, R.L. Keiski, *Top. Catal.* **54** (2011) 1224-1256.
- [2] P. Yang, S. Yang, Z. Shi, Z. Meng, R. Zhou, *Appl. Catal. B* **162** (2015) 227-235.
- [3] I. Maupin, L. Pinard, J. Mijoin, P. Magnoux, *J. Catal.* **291** (2012) 104-109.
- [4] S. Pitkaaho, L. Matejova, S. Ojala, J. Gaalova, R.L. Keiski, *Appl. Catal. B* **113-114** (2012) 150-159.
- [5] L. Jin, R. Ma, J. Lin, L. Meng, Y. Wang, M. Luo, *Ind. Eng. Chem. Res.* **50** (2011) 10878-10882.
- [6] X. Zhang, Z. Pei, X. Ning, H. Lu, H. Huang, *RSC ADVANCES* **5** (2015) 79192-79199.
- [7] M. Romero-Sáez, D. Divakar, A. Aranzabal, J.R. González-Velasco, J.A. González-Marcos, *Appl. Catal. B* **180** (2016) 210-218.
- [8] A. Aranzabal, M. Romero-Saez, U. Elizundia, J.R. Gonzalez-Velasco, J.A. Gonzalez-Marcos, *J. Catal.* **296** (2012) 165-174.
- [9] R.W. van den Brink, P. Mulder, R. Louw, *Catal. Today* **54** (1999) 101-106.
- [10] V. de Jong, M.K. Cieplik, W.A. Reints, F. Fernandez-Reino, R. Louw, *J. Catal.* **211** (2002) 355-365.
- [11] W. Cen, Y. Liu, Z. Wu, J. Liu, H. Wang, X. Weng, *J. Phys. Chem. C* **118** (2014) 6758-6766.
- [12] Q. Dai, X. Wang, G. Lu, *Appl. Catal. B* **81** (2008) 192-202.
- [13] X.Y. Wang, Q. Kang, D. Li, *Catal. Commun.* **9** (2008) 2158-2162.
- [14] B. de Rivas, R. Lopez-Fonseca, C. Sampedro, J.I. Gutierrez-Ortiz, *Appl. Catal. B* **90** (2009) 545-555.
- [15] H. Huang, Y. Gu, J. Zhao, X. Wang, *J. Catal.* **326** (2015) 54-68.
- [16] Y. Li, W. Shen, *Chem. Soc. Rev.* **43** (2014) 1543-1574.
- [17] K. Deori, C. Kalita, S. Deka, *J. Mater. Chem. A* **3** (2015) 6909-6920.
- [18] Y. Li, Z. Wei, F. Gao, L. Kovarik, C.H.F. Peden, Y. Wang, *J. Catal.* **315** (2014) 15-24.
- [19] M. Li, Z. Wu, S.H. Overbury, *J. Catal.* **306** (2013) 164-176.
- [20] Y. Gao, W. Wang, S. Chang, W. Huang, *Chem. Cat. Chem.* **5** (2013) 3610-3620.
- [21] Tana, M. Zhang, J. Li, H. Li, Y. Li, W. Shen, *Catal. Today* **148** (2009) 179-183.
- [22] Z. Hu, X. Liu, D. Meng, Y. Guo, Y. Guo, G. Lu, *ACS Catal.* (2016) 2265-2279.
- [23] W. Han, W. Wen, J.C. Hanson, X. Teng, N. Marinkovic, J.A. Rodriguez, *J. Phys. Chem. C* **113** (2009) 21949-21955.
- [24] R. Si, M. Flytzani-Stephanopoulos, *Angew. Chem. Int. Ed.* **47** (2008) 2884-2887.
- [25] H. Mai, L. Sun, Y. Zhang, R. Si, W. Feng, H. Zhang, H. Liu, C. Yan, *J. Phys. Chem. B* **109** (2005) 24380-24385.
- [26] Q.G. Dai, X.Y. Wang, G.Z. Lu, *Appl. Catal. B* **81** (2008) 192-202.
- [27] B. de Rivas, C. Sampedro, R. Lopez-Fonseca, M.A. Gutierrez-Ortiz, J.I. Gutierrez-Ortiz, *Appl. Catal. A* **417** (2012) 93-101.
- [28] W. Mišta, M.A. Małecka, L. Kępiński, *Appl. Catal. A: General* **368** (2009) 71-78.
- [29] H.C. Yao, Y.F.Y. Yao, *J. Catal.* **86** (1984) 254-265.
- [30] E. Beche, P. Charvin, D. Perarnau, S. Abanades, G. Flamant, *Surf. Interface Anal.* **40** (2008) 264-267.
- [31] Z. Wu, M. Li, J. Howe, H.M. Meyer, S.H. Overbury, *Langmuir* **26** (2010) 16595-16606.
- [32] P. Yang, Z. Meng, S. Yang, Z. Shi, R. Zhou, *J. Mol. Catal. A* **393** (2014) 75-83.
- [33] Q. Dai, S. Bai, Z. Wang, X. Wang, G. Lu, *Appl. Catal. B* **126** (2012) 64-75.
- [34] K. Sutthiumporn, S. Kawi, *Int. J. Hydrogen Energy* **36** (2011) 14435-14446.
- [35] P. Zhao, C. Wang, F. He, S. Liu, *RSC Advances* **4** (2014) 45665-45672.
- [36] Q. Dai, S. Bai, H. Li, W. Liu, X. Wang, G. Lu, *Appl. Catal. B* **168-169** (2015) 141-155.

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