



# Highly efficient CO<sub>2</sub> capture from open air and dilute gas streams by tunable azolate ionic liquids based deep eutectic solvents

Guokai Cui <sup>a,\*</sup> , Yepin Cheng <sup>a</sup>, Wei Zhang <sup>b</sup>, Xiangyu Shen <sup>a</sup>, Lai Li <sup>b</sup>, Ruina Zhang <sup>a</sup>, Yaoji Chen <sup>b</sup>, Quanli Ke <sup>a</sup> , Chunliang Ge <sup>b</sup>, Huayan Liu <sup>a</sup>, Wenyang Fan <sup>b</sup>, Hanfeng Lu <sup>a,\*</sup>

<sup>a</sup> Innovation Team of Air Pollution Control, Institute of Catalytic Reaction Engineering, Zhejiang Key Laboratory of Surface and Interface Science and Engineering for Catalysts, State Key Laboratory Breeding Base of Green Chemistry Synthesis Technology, College of Chemical Engineering, Zhejiang University of Technology, Hangzhou 310014, China

<sup>b</sup> Zhejiang Zheneng Technology & Environment Group Co., Ltd., Hangzhou 310012, China



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## ABSTRACT

A series of functional deep eutectic solvents (DESs) forming from azolate ionic liquids (ILs) and ethylene glycol (EG) or succinonitrile (SN) were designed and synthesized for CO<sub>2</sub> capture with ultra-high uptake from open air (420–430 ppm) or dilute gas streams (500 ppm–5 vol%). With the increase of pKa of azoles, the CO<sub>2</sub> capacity of these azolate-based DESs increased linearly with R<sup>2</sup> = 0.96. Compared with other DESs and ILs, the extremely high CO<sub>2</sub> capture capacities of 14 wt% (3.18 mmol/g), 25 wt% (5.68 mmol/g), and 26 wt% (5.91 mmol/g) could be reached under open air / 500 ppm, 2 vol%, and 5 vol% CO<sub>2</sub>, respectively, *via* tuning the structures of DESs. In addition, spectroscopic investigations revealed that the anion-induced multi-site cooperations of O···CO<sub>2</sub> and N···CO<sub>2</sub> were the reason of ultrahigh CO<sub>2</sub> capacities. To the best of our knowledge, these are the first examples of tuning amine-free functional DESs for the highly efficient CO<sub>2</sub> capture from open air. The significant improvements made in this work on CO<sub>2</sub> capture over conventional sorbents provide an alternative strategy for industrial gas capture and utilization *via* anion-induced multi-site cooperations.

## 1. Introduction

The increase concentration of CO<sub>2</sub> in the open air has been associated with global climate change and gives rise to direct air capture (DAC) technology.<sup>[1,2]</sup> Moreover, before the raw natural gas goes into pipeline, CO<sub>2</sub> concentration must be decreased below 2 % by carbon capture technologies to meet the US and most countries' pipeline standards to prevent corrosion and damage to equipment.<sup>[3]</sup> It is known that physical sorption and cryogenic separation can be applied for gas streams with higher CO<sub>2</sub> concentrations (typically > 50 %), while chemical sorption should be used for gas streams with lower CO<sub>2</sub> concentrations.<sup>[4,5]</sup> Conventional amine-based sorbents have been proved for efficient CO<sub>2</sub> capture for low-concentration CO<sub>2</sub> through chemical absorption. However, this technology results in high energy-consumption and high solvent-loss, as well as corrosion.<sup>[6]</sup> Thus, the designing and development of other highly efficient amine-free CO<sub>2</sub>-philic sorbents for CO<sub>2</sub> capture and separation from open air (420–430 ppm) or dilute gas streams (500 ppm–5 vol%) is necessary but challenging.

Composed of cations and anions, ionic liquids (ILs) have been used as

absorbents for the capture and separation of SO<sub>2</sub>,<sup>[7–11]</sup> NO<sub>x</sub>,<sup>[12–14]</sup> NH<sub>3</sub>,<sup>[15–17]</sup> CO,<sup>[18–20]</sup> and especially CO<sub>2</sub>,<sup>[21–26]</sup> etc. during these two decades due to their unique properties, including nonflammable, high thermo-stability, structural designability, etc.<sup>[27–31]</sup> However, the high viscosity limits the use of ILs for CO<sub>2</sub> in industry. For example, a saturated absorption capacity of 27 wt% CO<sub>2</sub> (6.1 mmol g<sup>-1</sup>) could be achieved by neat amine-functional IL 1-hydroxyethyl-3-methylimidazolium lysine ([C<sub>2</sub>OHmim][Lys]) after 60 h under 1 bar, with the state of IL changed from liquid to solid because of the strong chemical reactions.<sup>[32]</sup> In view of this, to avoid the effect of liquid viscosity on the liquid phase mass transfer, deep eutectic solvents (DESs),<sup>[33–35]</sup> composed of hydrogen bond acceptors (HBAs) and hydrogen bond donors (HBDs), have been developed for CO<sub>2</sub> capture as the alternative sorbents with the similar tunable physical-chemical properties as the ILs.<sup>[21,36]</sup> For example, Zhang *et al.*<sup>[37]</sup> reported a series of amine-functionalized DESs for CO<sub>2</sub> capture with 1-butyl-3-methylimidazolium chloride ([Bmim][Cl]) as the HBA and monoethanolamine (MEA) as the HBD (molar ratios 1:1, 1:2 and 1:4), and the CO<sub>2</sub> capacities of these DESs were 8.4, 17.9, and 21.4 wt%, respectively, at 25 °C and 1 bar, indicating the

\* Corresponding authors.

E-mail addresses: [chemcgk@163.com](mailto:chemcgk@163.com) (G. Cui), [luhf@zjut.edu.cn](mailto:luhf@zjut.edu.cn) (H. Lu).

larger the concentration of MEA, the higher the  $\text{CO}_2$  absorption capacity. However, these DESs will result in the problem of conventional amine-based sorbents. Ren *et al.* [38] showed that the  $\text{CO}_2$  capacities of functional DES based on triethylenetetramine hydrochloride ([TETAH] [Cl]) as the HBA and thymol (Thy) as the HBD with the molar ratio of 1:3 were 9 % and 4.1 % at 40 °C under 1 bar and 0.1 bar, respectively. However, the desorptions of  $\text{N}-\text{CO}_2$  carbamates formed via the reactions of amines and  $\text{CO}_2$  always need more than 100°C to release  $\text{CO}_2$  and obtain DESs. Besides, the viscosity of these functional DESs were dramatically increased after  $\text{CO}_2$  absorption. For example, the viscosities of [TETAH][Cl]:Thy (1:3) and  $\text{CO}_2$ -saturated [TETAH][Cl]:Thy (1:3) were 205.1 and  $6.77 \times 10^3$  mPa s, respectively. [38] Because of the azolate anion-functionalized ILs (AILs) could be used for efficient  $\text{CO}_2$  capture as well as the high  $\text{CO}_2$  absorption capacity and low absorption enthalpy of 1,2,4-triazolate ILs, [39–42] Yang *et al.* [43] reported that the  $\text{CO}_2$  absorption capacities of DESs with 1,2,4-triazolate IL-based HBAs and ethylene glycol (EG) HBA were around 12 % at 25 °C and 1 bar, as well as the completely desorption could be achieved at 70 °C under 1 bar  $\text{N}_2$ . Although some AIL-based DESs have been developed for  $\text{CO}_2$  capture, the  $\text{CO}_2$  absorption capacities were still low and the data were limited, especially for  $\text{CO}_2$  capture from open air or dilute gas streams. [44–47] Thus, novel sorbents with highly efficient capture of  $\text{CO}_2$  from open air and dilute gas streams are highly desired.

Herein, we designed and synthesized a series of amine-free AIL-based DESs. These DESs are AILs as the HBAs as well as EG and succinonitrile (SN) as the HBDs with the molar ratio of HBA:HBD = 2:1, 1:1 and 1:2, and the structure of these DESs can be found in Fig. 1. With adjusting the structures of DESs and considering the physical and chemical properties,  $\text{CO}_2$  capture by the functional DES formed with 1,5-diazabicyclo[4.3.0]non-5-enium pyrazolate ([DBNH][Pyrz]) as the HBA and EG as the HBD with molar ratio of HBA:HBD = 1:1 exhibited an ultrahigh  $\text{CO}_2$  capture capacities of 14 wt% (3.18 mmol g<sup>-1</sup>), 25 wt% (5.68 mmol g<sup>-1</sup>), and 26 wt% (5.91 mmol g<sup>-1</sup>) under open air / 500 ppm, 2 vol%, and 5 vol%  $\text{CO}_2$ , respectively. To the best of our knowledge, these capacities are superior than that of other DESs and ILs. Spectroscopic investigations revealed that the anion-induced multi-site cooperations of  $\text{O}\cdots\text{CO}_2$  and  $\text{N}\cdots\text{CO}_2$  were the reason of ultrahigh  $\text{CO}_2$  capacities.

## 2. Experimental methods

### 2.1. Materials

1,5-Diazabicyclo[4.3.0]non-5-ene (DBN, 98 wt%), pyrazole (Pyrz, 98 wt%), imidazole (Im, 98 wt%), 1,2,4-triazole (1,2,4-Triz, 98 wt%), 1,2,3-triazole (1,2,3-Triz, 98 wt%), tetrazole (Tetz, 98 wt%) were supplied by Shanghai Aladdin Biochemical Technology Co., Ltd. Tetraethylammonium hydroxide ([N<sub>2222</sub>][OH], 25 wt% in  $\text{H}_2\text{O}$ ) were obtained from Shanghai Titan Technology Co., Ltd. while ethylene glycol (EG, 99 wt%) was purchased from Shanghai Lingfeng Chemical Reagent Co., Ltd. and succinonitrile (SN, 99 wt%) was supplied by Shanghai Maclean Biochemical Technology Co., Ltd. All regents were used without further purification. The open air which contained about 420–430 ppm  $\text{CO}_2$  was used after it was dried with  $\text{CaO}$ . The gas

mixtures containing 500 ppm of  $\text{CO}_2$  was generated from mixing  $\text{CO}_2$  (0.5 vol%) and  $\text{N}_2$  (99.99 vol%), while the gas mixtures containing 1 vol %, 2 vol%, 3 vol%, and 4 vol% of  $\text{CO}_2$  was generated from mixing  $\text{CO}_2$  (5 vol%) and  $\text{N}_2$  (99.99 vol%) with the flow rates controlled by mass flow controllers (model: D07-19B, Beijing Sevenstar Electronics Co. Ltd., Beijing, China) with digital read out box (model: D08-3B/ZM, Beijing Sevenstar Electronics Co. Ltd, Beijing, China) and verified by soap bubble flowmeters.  $\text{CO}_2$  (0.5 vol%, 5 vol%, and 99.99 vol%) and  $\text{N}_2$  (99.99 vol%) were obtained from Hangzhou Jingong Special Gas Co., Ltd. All the  $\text{CO}_2$  concentrations (open air, 500 ppm, 0.5 vol%, 1 vol%, 2 vol%, 3 vol%, 4 vol% and 5 vol%) were measured / verified by a non-dispersive infrared  $\text{CO}_2$  analyzer (GXH-3010F, Beijing Huayun Analytical Instrument Institution Co., Ltd., China) with the accuracy of 0.001 % (<https://www.hyaii.com>).

### 2.2. Synthesis of functional DESs

All kinds of AILs, such as [DBNH][Pyrz], 1,5-diazabicyclo[4.3.0]non-5-enium imidazolate ([DBNH][Im]), 1,5-diazabicyclo[4.3.0]non-5-enium 1,2,4-triazolate ([DBNH][1,2,4,-Triz]), 1,5-diazabicyclo[4.3.0]non-5-enium 1,2,3-triazolate ([DBNH][1,2,3-Triz]), and 1,5-diazabicyclo[4.3.0]non-5-enium tetrazolate ([DBNH][Tetz]), as well as tetraethylammonium pyrazolate ([N<sub>2222</sub>][Pyrz]) were prepared by acid-base neutralization of DBN or [N<sub>2222</sub>][OH] with an appointed proton donor (Pyrz, Im, etc.) at 60 °C and atmospheric pressure for 6 h. All functional DESs were prepared through mixing HBAs and HBDs together in certain molar ratios. For example, in a typical synthesis of [DBNH][Pyrz]:EG (1:1), [DBNH][Pyrz] (0.04 mol, 7.69 g) and EG (0.04 mol, 2.48 g) were added together in a round-bottom flask under an atmosphere of  $\text{N}_2$ . The mixture was stirred at 60 °C for 2 h until turning into a homogeneous and transparent liquid. Then, these DESs dried under vacuum at 60 °C for at least 24 h to remove the reduce the possible trace of water before used.

### 2.3. Characterization

The chemical structures of these functional DESs before and after the absorption of  $\text{CO}_2$  were verified by NMR and FT-IR methods at room temperature, and the instruments were supplied by Bruker (400 MHz NMR and VERTEX 70 IR). Deuteriochloroform ( $\text{CDCl}_3$ ) and dimethyl sulfoxide-d<sub>6</sub> (DMSO-d<sub>6</sub>) was used as the solvent and residual  $\text{CHCl}_3$  (77.16 ppm) and DMSO (39.50 ppm) can be recognized as the internal reference for NMR analyzing. High-resolution mass spectrometry (HR-MS, Thermo Fisher Scientific Q Exactive Focus, Bruker Esquire 3000) equipped with electrospray ionization (ESI) interface and ion-trap analyzer was used to analyze the ionic compounds (ILs and DESs) and obtain the molecular weight (Mw) of ions. The melting points were measured on a NETZSCH DSC 200F3 in the range of –100 to 40 °C at a heating rate of 10 °C min<sup>-1</sup> under  $\text{N}_2$  atmosphere. Using an EG-calibrated pycnometer, densities of DESs were measured in the temperature range of 20–80 °C with an interval of 10 °C under atmospheric pressure. The viscosities of these DESs were determined at the same temperatures using a viscometer supplied from Brookfield (DVNEXT-LV).

### 2.4. $\text{CO}_2$ capture

The experiments of  $\text{CO}_2$  absorption by these functional DESs were carried out according to previous report [43] under atmospheric pressure at various temperatures and different concentration  $\text{CO}_2$  in dilute gas streams. In a typical run of  $\text{CO}_2$  absorption, gas with different concentration of  $\text{CO}_2$  was bubbled into about 1.0 g DES in a glass container with an inner diameter of 10 mm, which was partly immersed in a metal bath of desirable temperature. The flow rate was controlled at about 20 mL min<sup>-1</sup> using a rotameter (Xinghua Xiangjin Flow Meter Factory, Xinghua, China) with the accuracy of ±6 %, while the standard

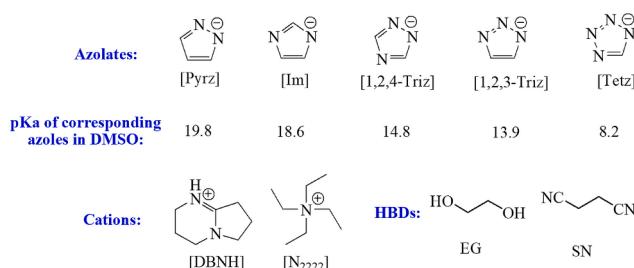


Fig. 1. Structures of anions, cations, and HBDs in this work.

uncertainty of absorption temperature  $u(T)$  is  $\pm 0.1$  °C. An electronic balance with the accuracy of  $\pm 0.0001$  g was used to measure the  $\text{CO}_2$  absorption capacities by different DESs at regular intervals. To test the reliability of our absorption equipment and method,  $[\text{P}_{2222}][1,2,4\text{-Triz}]:\text{EG}$  (1:2) was prepared and  $\text{CO}_2$  capture was measured under the same conditions (25 °C and 1 bar  $\text{CO}_2$ ) as the reference [43]. The results of comparison exhibited no obvious change of capacity between our absorption data and the data in the reference [43], indicating the absorption equipment and method were reliable (Fig. S1). Besides, a process for  $\text{CO}_2$  capture from open air ( $\text{CO}_2$  concentration: 420–430 ppm) is developed and illustrated in Fig. 2, and the absorption experiments were carried out as similar as  $\text{CO}_2$  capture from dilute gas streams. The absorption capacity of  $\text{CO}_2$  by DES ( $Z$ , in mole of  $\text{CO}_2$  per mole of anion) was calculated according to the literatures:

$$Z = \frac{(m_{\text{total}} - m_{\text{DES}})/M_{\text{CO}_2}}{m_{\text{DES}}/M_{\text{DES}}} \times \frac{1}{n_{\text{HBA}}}$$

where  $M_{\text{CO}_2}$  and  $M_{\text{DES}}$  are the molar weights of  $\text{CO}_2$  and DES in g mol<sup>-1</sup>, respectively.  $M_{\text{DES}}$  could be calculated  $M_{\text{DES}} = n_{\text{HBA}} \times M_{\text{HBA}} + n_{\text{HBD}} \times M_{\text{HBD}}$ , where  $M_{\text{HBA}}$  and  $M_{\text{HBD}}$  are the molar weights of HBA and HBD in g mol<sup>-1</sup>, and  $n_{\text{HBA}}$ :  $n_{\text{HBA}}$  is the molar ratio of HBA: HBD.

### 3. Results and discussion

#### 3.1. Physical properties

First of all, the molecular ion peak, including cation and anion, of typical ILs [DBNH][Pyrz] and [DBNH][1,2,3-Triz], and corresponding DESs, [DBNH][Pyrz]:EG (1:1) and [DBNH][1,2,3-Triz]:EG (1:1) were determined with HR-ESIMS under positive ion mode or negative ion mode, and the results were illustrated in Fig. S2. For example, it could be seen that an ion peak at  $m/z$  125.107 in HR-ESIMS spectrum of [DBNH][Pyrz] under positive ion mode could be assigned to [DBNH] cation (Mw of DBN is 124.18 g mol<sup>-1</sup>) while an ion peak at  $m/z$  67.029 under negative ion mode could be assigned to [Pyrz] anion (Mw of Pyrz 68.08 g mol<sup>-1</sup>), indicating the formation of [DBNH] cation and [Pyrz] anion via acid-base neutralization. Clearly, these peaks both available in the spectra of [DBNH][Pyrz]:EG (1:1) while unavailable in the spectra of DBN-EG (1:1), suggesting the introduction of EG in IL may not affect the structure and ionicity of [DBNH][Pyrz] and the EG (Mw = 62.07 g mol<sup>-1</sup>) could not be deprotonated in [DBNH][Pyrz]:EG (1:1). Moreover, the melting points of typical ILs and corresponding IL-based DESs were measured, and the results were illustrated in Fig. S3. It is showed that the melting points of [DBNH][Pyrz]:EG (1:1), and [DBNH][1,2,4-Triz]:EG (1:1) are all lower than [DBNH][Pyrz] and [DBNH][1,2,4-Triz], respectively, indicated that these IL-based mixtures were DESs, according to the definition of DESs.

Affected by the structures of DESs and the molar ratios of HBA:HBD,

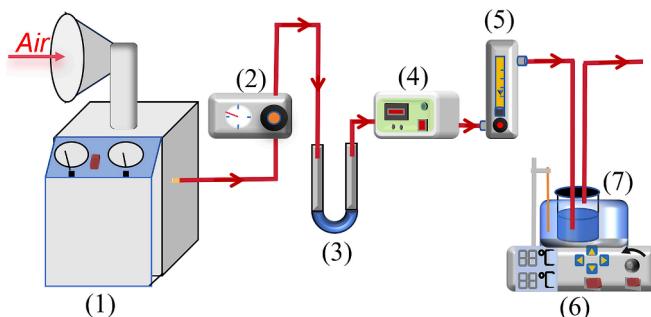


Fig. 2. Apparatus of  $\text{CO}_2$  capture from open air: (1) Air generator containing  $\text{CO}_2$ ; (2) high pressure valve; (3) drying tube with anhydrous  $\text{CaCl}_2$ ; (4)  $\text{CO}_2$  analyzer; (5) rotameter; (6) magnetic stirrer with thermocouple; (7) glass bottle filled with DES.

it is clear that density and viscosity are vital rheological properties of a mixture and will affect the  $\text{CO}_2$  capture performance. [48–50] Thereby, these properties of [DBNH][Pyrz]:EG 1:1), [DBNH][Im]:EG (1:1), [DBNH][Pyrz]:SN (1:1), and  $[\text{N}_{2222}][\text{Pyrz}]:\text{EG}$  (1:1) were measured at different temperatures in the range of 20 °C ~ 80 °C under atmospheric pressure, and the values are listed in Table S1. It can be seen that the density ( $\rho$ , in g cm<sup>-3</sup>) and viscosity ( $\eta$ , in mPa·s) are inversely proportional to temperature. With the temperature increase, both the density and the viscosity decreased, and vice versa, due to the increase in volume. The values of density were around 1 g cm<sup>-3</sup> while that of the viscosity were in a large range of 159.4–1.48 mPa·s. Clearly, the lowest density and the largest viscosity could be found in  $[\text{N}_{2222}][\text{Pyrz}]:\text{EG}$  (1:1) at any temperature, indicating these properties are greatly influenced by the structures of DESs. The relations between density and temperature and between viscosity and temperature could be described by the following linear equations, respectively.

$$\ln \rho = a + b T$$

and

$$\ln \eta = \ln \eta_0 + \frac{E_\eta}{RT}$$

where  $a$  and  $b$  are fitting constants,  $\eta_0$  denotes the pre-exponential constant in mPa·s,  $E_\eta$  represents the flow activation energy in kJ mol<sup>-1</sup>,  $T$  is the experimental temperature in K, and  $R$  is the universal gas

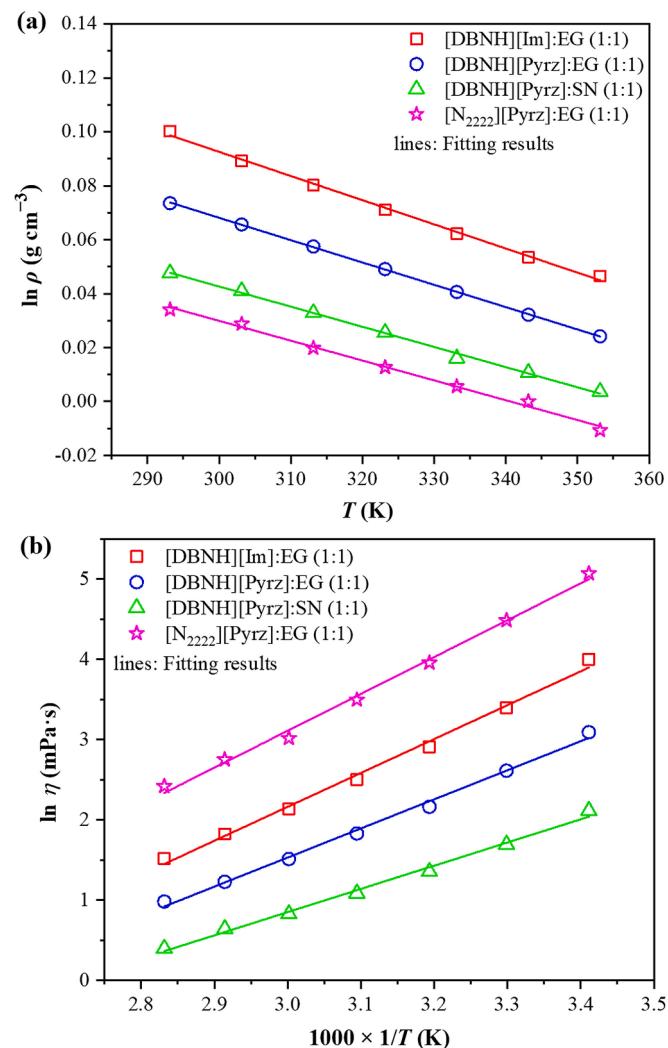


Fig. 3. Linear relationship for density (a) and viscosity (b) with the temperature.

constant ( $8.314 \text{ J K}^{-1} \text{ mol}^{-1}$ ). The fitting curves were illustrated in Fig. 3 and the parameters were listed in Table S2. The fitting results showed that the values of  $E_\eta$  decreased in the order:  $[\text{N}_{2222}][\text{Pyrz}]:\text{EG}$  (1:1) >  $[\text{DBNH}][\text{Im}]:\text{EG}$  (1:1) >  $[\text{DBNH}][\text{Pyrz}]:\text{EG}$  (1:1) >  $[\text{DBNH}][\text{Pyrz}]:\text{SN}$  (1:1). Coefficient of thermal expansion of DESs ( $\alpha_p$ , in  $\text{K}^{-1}$ ) is the rate at which the volume of a DES ( $V$ , in  $\text{cm}^3 \text{ mol}^{-1}$ ) changes with respect to the temperature ( $T$ , in K) change, as the following equation:

$$\alpha_p = \frac{1}{V} \times \left(\frac{\partial V}{\partial T}\right)_p = - \left(\frac{\partial \ln \rho}{\partial T}\right)_p$$

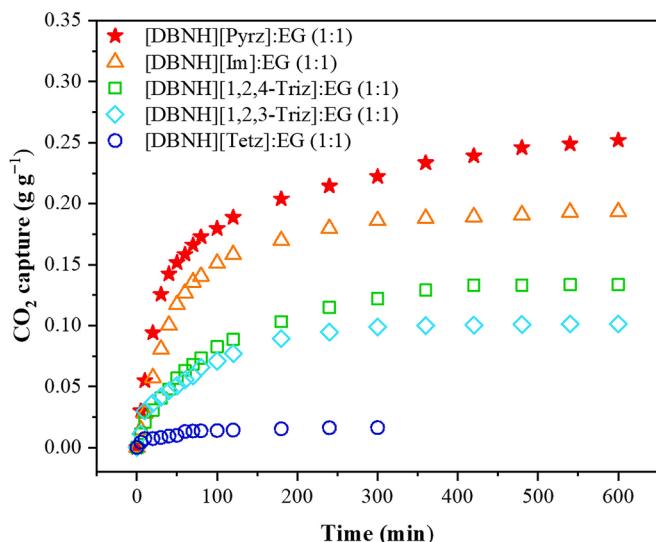
The values of  $\alpha_p$  were listed in Table S3. Clearly, the values of  $\alpha_p$  decreased in the order: [DBNH][Im]:EG (1:1) > [DBNH][Pyrz]:EG (1:1) > [DBNH][Pyrz]:SN (1:1) > [N<sub>2222</sub>][Pyrz]:EG (1:1). The higher thermal coefficient value indicates higher free volume of fluids.

### 3.2. *CO<sub>2</sub> capture*

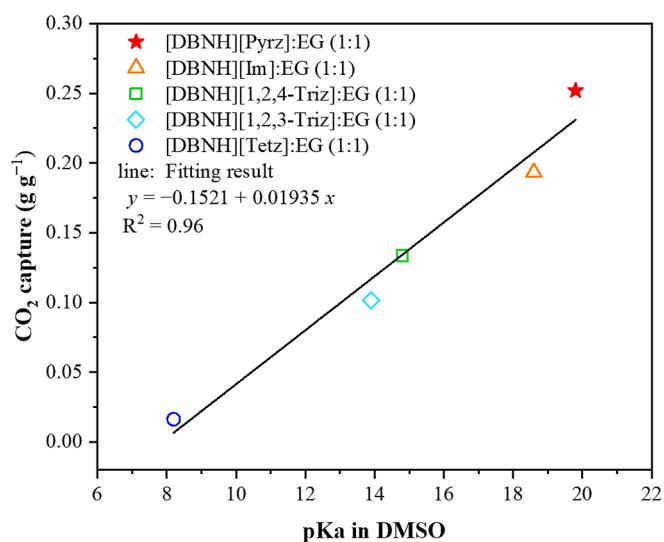
### 3.2.1. Effects of structures of DESSs

A DES includes three parts, cation, anion, and HBD. Thus, the structures of cation, anion and HBD inevitably affect the performance of CO<sub>2</sub> capture by DESs. As the anion plays a key role in CO<sub>2</sub> capture by ILs, the effect of anion with different structures was first investigated and the results were illustrated in Fig. 4. It can be seen that the CO<sub>2</sub> capture capacities of [DBNH][Pyrz]:EG (1:1), [DBNH][Im]:EG (1:1), [DBNH][1,2,4-Triz]:EG (1:1), [DBNH][1,2,3-Triz]:EG (1:1), and [DBNH][Tetz]:EG (1:1) were 26 wt% (5.91 mmol g<sup>-1</sup>), 19 wt% (4.32 mmol g<sup>-1</sup>), 13 wt% (2.95 mmol g<sup>-1</sup>), 10 wt% (2.27 mmol g<sup>-1</sup>), and 2 wt% (0.45 mmol g<sup>-1</sup>) at 20 °C under 5 vol% CO<sub>2</sub>, respectively. It is known that the structure of azoles, including the position and the amount of N atoms, affect the basicity of azolate anions. Thus, the relationship between pKa of azoles and the CO<sub>2</sub> capture capacities of these azolate-based DESs was further studied, and the result was revealed in Fig. 5 and Table S4. With the increase of pKa of azoles, the CO<sub>2</sub> capacity of these azolate-based DESs increased linearly with  $R^2 = 0.96$ . That is, [DBNH][Pyrz]:EG (1:1) obtained the highest CO<sub>2</sub> capacity because of the pyrazole with the highest pKa value (19.8 in DMSO). Besides, it is safely predicted that anions with pKa < 7.9 in DMSO would not absorb CO<sub>2</sub> at all. This value near the pKa of carbonic acid (pKa = 6.36 in H<sub>2</sub>O and aqueous pKa < DMSO pKa by 1 ~ 13 units).<sup>[51]</sup> There by, pyrazolate anion was selected for the following investigations.

The molar ratio of HBA:HBD is not only affects the density and viscosity of DES, but also affects the  $\text{CO}_2$  absorption capacity. Thus, the performances of  $\text{CO}_2$  capture by  $[\text{DBNH}][\text{Pyrz}]:\text{EG}$  (2:1),  $[\text{DBNH}]$



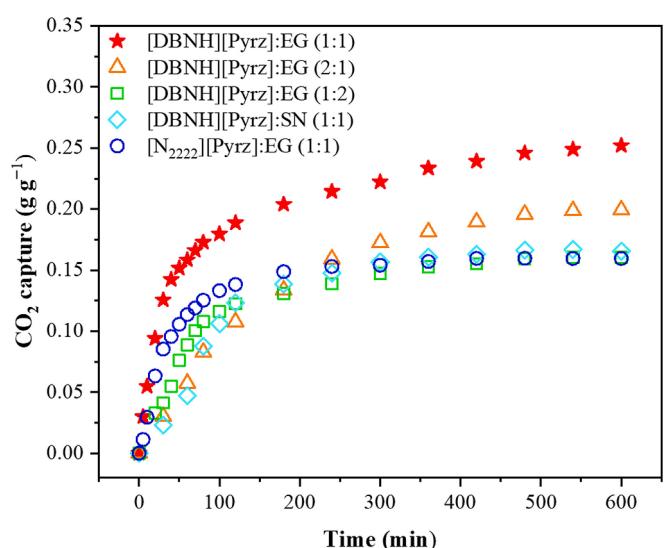
**Fig. 4.** Effect of structures of azolate anion on the CO<sub>2</sub> absorption by DESs at 20 °C under 5 vol% CO<sub>2</sub>.



**Fig. 5.** Relationship between pKa of azoles and the CO<sub>2</sub> capture capacities of DESs.

[Pyrz]:EG (1:1), and [DBNH][Pyrz]:EG (1:2) were investigated, and the results were illustrated in Fig. 6. It can be seen that the capacities of these DESs were 20 wt% (4.55 mmol g<sup>-1</sup>), 26 wt% (5.91 mmol g<sup>-1</sup>), and 16 wt% (3.64 mmol g<sup>-1</sup>) at 20 °C under 5 vol% CO<sub>2</sub>, respectively. The results indicated that the concentration of IL cannot be too high or too low, possibly because of the reaction mechanism. In addition, CO<sub>2</sub> capacity of [DBNH][Pyrz]:SN (1:1) was only 17 wt% (3.86 mmol g<sup>-1</sup>) at 20 °C under 5 vol% CO<sub>2</sub>, indicating the hydroxyl groups in the EG is also the active sites for CO<sub>2</sub> capture by AIL-based DESs. Moreover, an aprotic cation tetrabutylammonium ([N<sub>2222</sub>]<sup>+</sup>) was selected to test the effect of the structure of cation in DES on CO<sub>2</sub> capture. The results also could be found in Fig. 6. CO<sub>2</sub> capacity of [N<sub>2222</sub>][Pyrz]:EG (1:1) was also 16 wt% at 20 °C under 5 vol% CO<sub>2</sub>, indicating the proton on the cation is beneficial for CO<sub>2</sub> absorption.

Moreover, the viscosities of [DBNH][Pyrz]:EG (2:1), [DBNH][Pyrz]:EG (1:1), [DBNH][Pyrz]:EG (1:2) and [DBNH][Pyrz]:SN (1:1) DESs and their correspondent neat IL [DBNH][Pyrz] before and after  $\text{CO}_2$  saturation at 20 °C under 5 vol%  $\text{CO}_2$  were also measured to investigate the effect of EG and SN, the results were illustrated in Table 1. It can be seen



**Fig. 6.** Effect of molar ratio of HBA:HBD and the structures of cations and HBAs on the performance of  $\text{CO}_2$  absorption by DESs at 20 °C under 5 vol%  $\text{CO}_2$ .

**Table 1**

Comparison of viscosity of DESs and neat IL before and after  $\text{CO}_2$  saturation at 20 °C under 5 vol%  $\text{CO}_2$ .

Absorbent <sup>a</sup>	Viscosity (mPa s)		Viscosity Increase (fold) <sup>b</sup>	CO <sub>2</sub> Capacity		
	Before CO <sub>2</sub> capture	After CO <sub>2</sub> capture		mmol/g	g/g	mol/mol <sup>c</sup>
[DBNH]:[Pyrz]:EG (2:1)	26.56	407.7	15.35	4.55	0.20	1.02
[DBNH]:[Pyrz]:EG (1:1)	22.03	263.2	11.95	5.91	0.26	1.50
[DBNH]:[Pyrz]:EG (1:2)	28.05	116.5	4.15	3.64	0.16	1.31
[DBNH]:[Pyrz]:SN (1:1)	8.28	88.6	10.7	3.86	0.17	1.05
[DBNH]:[Pyrz]	12.23	1032	84.38	2.63	0.16	0.70

<sup>a</sup> Molar ratio in brackets.

<sup>b</sup> Viscosity of the absorbents saturated with  $\text{CO}_2$  relative to  $\text{CO}_2$ -free absorbents.

<sup>c</sup>  $\text{CO}_2$  capacity in mol/mol, meaning mole of  $\text{CO}_2$  per mole of [Pyrz] anion.

that the increased viscosity could be obtained for [DBNH]:[Pyrz]:EG DESs while the decreased viscosity could be obtained for [DBNH]:[Pyrz]:SN, due to the strong hydrogen bonding of formers. After  $\text{CO}_2$  saturation, the viscosity of all absorbents increased, and the increased folds for ILs are more than DESs, due to the strong interaction between cation and anion in formers. Besides,  $\text{CO}_2$  capacity of neat IL [DBNH]:[Pyrz] was only 6 wt% (3.86 mmol g<sup>-1</sup>) while that of [DBNH]:[Pyrz]-based DESs was more than 15 wt% (3.42 mmol g<sup>-1</sup>). While for  $\text{CO}_2$  capture in the unit of mol/mol (mole of  $\text{CO}_2$  per mole of [Pyrz] anion), the results indicated that suitable HBD (EG with molar ratio of [DBNH]:[Pyrz]:EG = 1:1) could promote the absorption of  $\text{CO}_2$ . Fig. 7 illustrated the  $\text{CO}_2$  absorption by three kinds of absorbents, a switchable solvent DBN-EG (1:1), an IL [DBNH]:[Pyrz], and a DES [DBNH]:[Pyrz]:EG (1:1). It can be seen that  $\text{CO}_2$  capacity of [DBNH]:[Pyrz]:EG (1:1) is 26 wt% (5.91 mmol g<sup>-1</sup>) while that of DBN-EG (1:1) is 0.21 wt% (4.77 mmol g<sup>-1</sup>), indicating that the introduction of Pyrz and formation of [Pyrz] could actually increase the  $\text{CO}_2$  absorption capacity per unit mass (g/g) of the absorbent. Additionally, the absorption capacity per unit molar (mol/mol) reflecting the reactivity of solvents, and the  $\text{CO}_2$  capacities of [DBNH]:[Pyrz]:EG (1:1) and DBN-EG (1:1) were 1.50 and 0.91 mol of  $\text{CO}_2$  per mole of solvent, also indicating the introduction of Pyrz and formation of [Pyrz] anion is efficient for  $\text{CO}_2$  capture. Thus, suitable EG and formation of [Pyrz] in [DBNH]:[Pyrz]:EG (1:1) system are both play a key role in  $\text{CO}_2$  capture. Based on the comprehensive considerations, [DBNH]:[Pyrz]:EG (1:1) DES was selected for future investigations.

### 3.2.2. Effects of $\text{CO}_2$ partial pressure and temperature

The performances of  $\text{CO}_2$  capture by [DBNH]:[Pyrz]:EG (1:1) under different  $\text{CO}_2$  partial pressures, particularly in the range of 500 ppm ~ 5 vol%  $\text{CO}_2$  ( $\text{CO}_2$  partial pressure 0.0005–0.05 bar), were studied. It is shown in Fig. 8 that the saturated  $\text{CO}_2$  capture capacity at 20 °C and 0.05 bar was 26 wt%  $\text{CO}_2$ . As the  $\text{CO}_2$  partial pressure decreased to 0.01 bar, the  $\text{CO}_2$  absorption capacity of 23 wt% (5.23 mmol g<sup>-1</sup>) could still be reached, indicating the efficient  $\text{CO}_2$  absorption of these DESs. To the best of our knowledge, these are the highest capacities for  $\text{CO}_2$  absorption by DESs and ILs under low concentrations of  $\text{CO}_2$  (Table 2). Recently, it is reported that the concentration of  $\text{CO}_2$  reached 413.2 ± 0.2 ppm by 2021 [52] and will increase to 500 ppm by 2050. [53] Thus, 500 ppm  $\text{CO}_2$  was used to test whether the [DBNH]:[Pyrz]:EG (1:1) DES is suitable for the direct capture of  $\text{CO}_2$  from ambient air, or "direct air

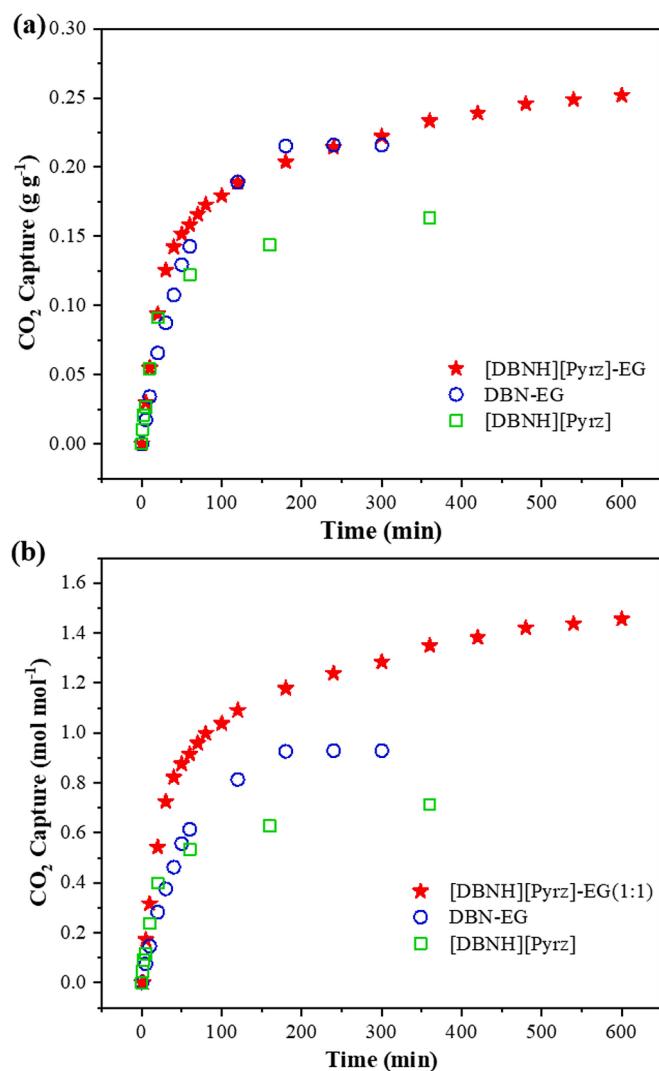


Fig. 7.  $\text{CO}_2$  absorption by [DBNH]:[Pyrz]:EG (1:1), DBN-EG (1:1), and [DBNH]:[Pyrz] at 20 °C under 5 vol%  $\text{CO}_2$ .

capture" (DAC) [54–56]. The results showed that as high as 14 wt% (3.18 mmol g<sup>-1</sup>)  $\text{CO}_2$  could be captured at 20 °C and 0.0005 bar  $\text{CO}_2$ , indicating the [DBNH]:[Pyrz]:EG (1:1) DES could be used as an alternative sorbent for DAC application. Moreover, the effect of absorption temperature on the  $\text{CO}_2$  absorption by [DBNH]:[Pyrz]:EG (1:1) was investigated and the results were also illustrated in Fig. 8.  $\text{CO}_2$  absorption capacity was found to be decreased with the increase of absorption temperature. For example, when the absorption temperature increased from 20 °C to 60 °C, the  $\text{CO}_2$  absorption capacity decreased from 26 wt% to 10 wt% (2.27 mmol g<sup>-1</sup>) under 0.05 bar  $\text{CO}_2$ . Additionally,  $\text{CO}_2$  capture from open air with the  $\text{CO}_2$  concentration between 420 to 430 ppm has been investigated, and the results were listed in Table 3. It can be seen that higher  $\text{CO}_2$  capacities could be obtained by [DBNH]:[Pyrz]:EG (1:1), [N<sub>2222</sub>]:[Pyrz]:EG (1:1), and [DBNH]:[Im]:EG (1:1), while lower capacities were obtained by [DBNH]:[1,2,3-Triz]:EG (1:1) and [DBNH]:[1,2,4-Triz]:EG (1:1), probably due to the high basicity of Pyrz and Im but low basicity of 1,2,3-Triz and 1,2,4-Triz, which consisted with the relationship between pKa of azoles and the  $\text{CO}_2$  capture capacities of DESs.

Above results indicated that the absorbed  $\text{CO}_2$  could be released and the DES could be recycled via either heating or bubbling  $\text{N}_2$  through the  $\text{CO}_2$ -saturated DES. Thus, the desorption of captured  $\text{CO}_2$  from  $\text{CO}_2$ -saturated [DBNH]:[Pyrz]:EG (1:1) and the recycle of [DBNH]:[Pyrz]:EG (1:1) have been investigated (Fig. 9). It can be seen from Fig. 9a that  $\text{CO}_2$

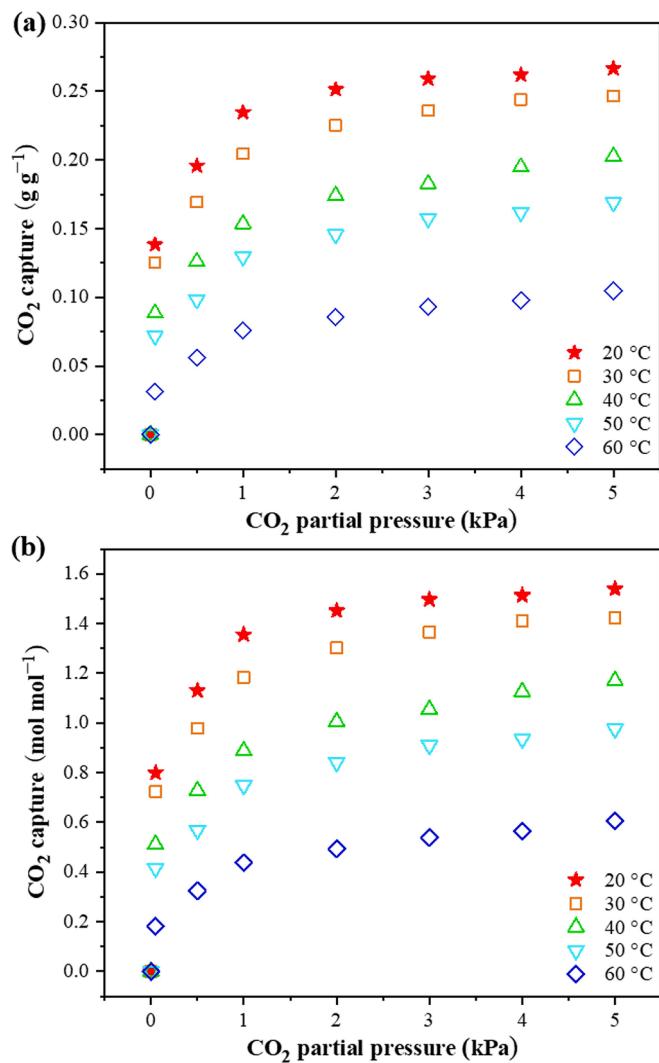


Fig. 8. CO<sub>2</sub> capture by [DBNH][Pyrz]:EG (1:1) under different CO<sub>2</sub> partial pressures and absorption temperatures.

could be desorbed at 60 °C under N<sub>2</sub>, which is milder than the desorption conditions reported in most previous work. The [DBNH][Pyrz]:EG (1:1) DES could be recycled seven times and the CO<sub>2</sub> capacity could be maintained (Fig. 9b).

### 3.2.3. Possible mechanism of CO<sub>2</sub> absorption

The mechanism of CO<sub>2</sub> absorption by [DBNH][Pyrz]:EG (1:1) was systematically studied. Fig. 10 shows the change of <sup>13</sup>C NMR spectroscopy of [DBNH][Pyrz]:EG (1:1) before and during the CO<sub>2</sub> absorption at 20 °C under 0.05 bar. Compared with the <sup>13</sup>C NMR spectrum of fresh [DBNH][Pyrz]:EG (1:1), when 5 wt% (1.14 mmol g<sup>-1</sup>) CO<sub>2</sub> was captured, a strong signal at 158.4 ppm and a weak signal at 158.0 ppm were produced. Interestingly, these signals were moved first down-field when 10 wt% CO<sub>2</sub> was captured and then up-field to 158.3 and 157.8 ppm when 15 wt% CO<sub>2</sub> was captured, indicating a change in the chemical environment surrounding these carbon atoms. It is clear that another new signal at 160.5 ppm was produced when 15 wt% CO<sub>2</sub> was captured. The intensity of the former two signals were slightly decreased while the latter one signal was slightly increased during more CO<sub>2</sub> absorbed in [DBNH][Pyrz]:EG (1:1). At last, the former signals appeared at 158.8 and 158.4 ppm while the latter signal appeared at 161.0 ppm in the <sup>13</sup>C NMR spectrum of CO<sub>2</sub>-saturated [DBNH][Pyrz]:EG (1:1). Based on the previous reports, [43,62,68,72] all these three signals would be attributed to carbonyl carbons of O···CO<sub>2</sub> carbamate species and/or

Table 2

Comparison of CO<sub>2</sub> capacities of [DBNH][Pyrz]:EG (1:1) with other DESs and ILs.

Absorbent <sup>a</sup>	T (°C)	P (bar)	CO <sub>2</sub> Capacity		Ref.
			(mmol/g)	(g/g)	
[DBNH][Pyrz]:EG (1:1)	40	0.05	4.55	0.20	This work
[DBNH][Pyrz]:EG (1:1)	30	0.05	5.68	0.25	This work
[DBNH][Pyrz]:EG (1:1)	20	0.05	5.91	0.26	This work
[DBNH][Pyrz]:EG (1:1)	20	0.02	5.68	0.25	This work
[DBNH][Pyrz]:EG (1:1)	20	0.01	5.23	0.23	This work
[DBNH][Pyrz]:EG (1:1)	20	0.0005	3.18	0.14	This work
[DBNH][Pyrz]:EG (1:1)	20	open air	3.18	0.14	This work
DBN:[Bmim][Cl]:Im (1:1:2)	25	1	2.46	0.1082	[57]
DBN:[Bmim][Cl]:Im (1:2:1)	25	1	1.79	0.0788	[57]
DBN:[Bmim][Cl]:Im (1:1:1)	25	1	2.78	0.1223	[57]
[Bmim][Cl]:MEA (1:1)	25	1	1.91	0.084	[37]
[DEAH][Cl]:MDEA (1:3)	25	1	2.46	0.1082	[58]
[MEA][Cl]:MEA (1:4)	20	1	5.68	0.25	[59]
[Ch][Cl]:MEA (1:5)	30	1	5.73	0.2523	[60]
[MDEAH][Cl]:MDEA (1:3)	25	1	1.35	0.0594	[58]
[N <sub>2222</sub> ][Thy]:EG (1:2)	25	1	2.23	0.0981	[61]
[N <sub>2222</sub> ][Car]:EG (1:2)	25	1	2.15	0.0948	[61]
[DBUH][Car]:EG (1:2)	25	1	2.27	0.1000	[62]
[DBUH][Thy]:EG (1:2)	25	1	2.27	0.1000	[62]
[TETAH][Cl]:thymol (1:3)	40	1	2.05	0.09	[38]
[TETAH][Cl]:thymol (1:3)	40	0.1	0.93	0.0411	[38]
[TEPAH <sub>2</sub> ][Im] <sub>2</sub> :EG (1:4)	25	1	3.95	0.1736	[63]
[DETAH <sub>2</sub> ][Im] <sub>2</sub> :EG (1:2)	25	1	5.08	0.2235	[63]
[P <sub>2222</sub> ][Triz]:EG (1:2)	25	1	2.68	0.118	[43]
[N <sub>2222</sub> ][Triz]:EG (1:2)	25	1	2.84	0.125	[43]
[Emim][2-CNpyr]:EG (1:2)	25	1	2.59	0.114	[64]
[Emim][Gly] + [Emim][Ac] (1:1)	25	1	2.95	0.13	[65]
[Emim][Gly] + [Emim][Ac] (1:1)	25	0.15	2.05	0.09	[65]
[DMAPAH][Ac] + EDA <sup>b</sup>	30	1	5.91	0.260	[66]
[DMAPAH][Ac] + EDA <sup>b</sup>	30	0.1	4.70	0.207	[66]
[MTBDH][Im]	23	1	4.65	0.20	[67]
[P <sub>66614</sub> ][Pyrz]	23	1	1.85	0.08	[40]
[P <sub>66614</sub> ][2-PyO]	20	1	2.73	0.12	[68]
[P <sub>4442</sub> ] <sub>2</sub> [IDA]	40	1	2.85	0.13	[25]
[P <sub>4442</sub> ][Suc]	20	1	5.68	0.25	[69]
[P <sub>4442</sub> ][Suc]	20	0.1	5.01	0.22	[69]
[N <sub>1111</sub> ][Eaca]	40	1	4.09	0.18	[70]
[N <sub>1111</sub> ][Eaca]	40	0.1	2.95	0.13	[70]
[Cho][Triz]	40	1	3.41	0.15	[71]
[P <sub>4446</sub> ][Im]	30	0.0004	1.92	0.08	[23]
[P <sub>4446</sub> ][BenIm]	30	0.0004	1.31	0.06	[23]

<sup>a</sup> molar ratio in brackets.

<sup>b</sup> mass ratio 1:1.

N···CO<sub>2</sub> carbamate species. Firstly, the signal at 158.4 ppm can be assigned to the carbonyl carbon of O···CO<sub>2</sub> in [EG – CO<sub>2</sub>] anion formed between the reaction of [EG] anion and CO<sub>2</sub>, and the [EG] anion was produced through deprotonation of EG by [Pyrz]. The signals of EG, [EG], and [EG – CO<sub>2</sub>] were in the range of 60 ~ 67 ppm. It can be seen that 63.0 ppm for the carbon of two same methylene groups in EG in the spectrum of fresh DES has been shifted to 62.8 ppm as well as two other new signals at 66.3 and 60.7 ppm were appeared after the absorption of 5 wt% CO<sub>2</sub>, attributing to two different carbons of methylene groups in unsymmetrical carbonate [EG – CO<sub>2</sub>] anion. Secondly, it is interesting that the signal at 158.0 ppm, accompanied by the signal at 158.4 ppm, in the <sup>13</sup>C NMR spectrum of DES + CO<sub>2</sub> (5 wt%), might be expected the

**Table 3**

CO<sub>2</sub> capture from open air (CO<sub>2</sub> concentration between 420 to 430 ppm) at 20 °C.

Absorbent <sup>a</sup>	Time (h)	CO <sub>2</sub> Capacity		
		mmol/g	g/g	mol/mol <sup>c</sup>
[DBNH][Pyrz]:EG (1:1)	48	3.18	0.14	0.81
[N <sub>2222</sub> ][Pyrz]:EG (1:1)	24	2.73	0.12	0.71
[DBNH][Im]:EG (1:1)	48	2.05	0.09	0.52
[DBNH][1,2,3-Triz]:EG (1:1)	24	1.14	0.05	0.29
[DBNH][1,2,4-Triz]:EG (1:1)	24	0.91	0.04	0.23

<sup>a</sup> Molar ratio in brackets.

<sup>c</sup> CO<sub>2</sub> capacity in mol/mol, meaning mole of CO<sub>2</sub> per mole of anion.

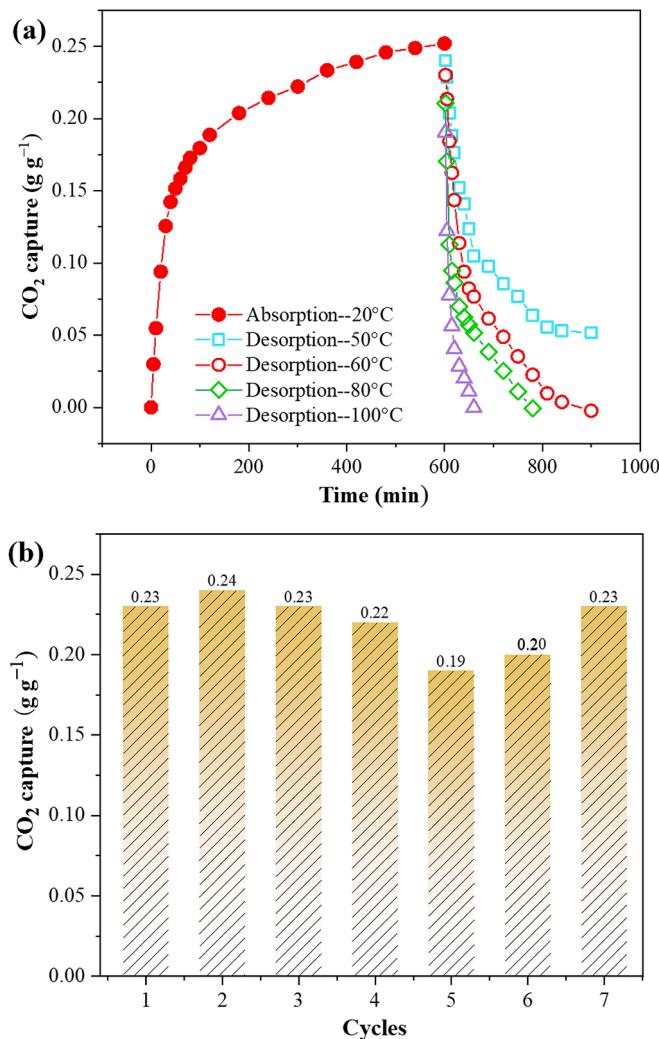


Fig. 9. (a) The desorption of captured CO<sub>2</sub> from CO<sub>2</sub>-saturated [DBNH][Pyrz]:EG (1:1) and (b) the recycle of [DBNH][Pyrz]:EG (1:1).

formation of symmetrical bicarbonate [CO<sub>2</sub> – EG – CO<sub>2</sub>]<sup>2-</sup> anion. [73] Another evidence for [CO<sub>2</sub> – EG – CO<sub>2</sub>]<sup>2-</sup> anion formation was that a new signal at 63.6 ppm appeared in the spectrum of [DBNH][Pyrz]:EG (1:1) after the absorption of 5 wt% CO<sub>2</sub>, different from the signal at 63.0 ppm in the spectrum of fresh [DBNH][Pyrz]:EG (1:1). It can be seen that the intensity of both shifts at 158.0 and 63.6 ppm first increased and then decreased simultaneously during the absorption of more CO<sub>2</sub>. Thirdly, the signal at 160.5 ppm appeared in the spectrum of DES after the absorption of 15 wt% CO<sub>2</sub> can be assigned to the carbonyl carbon of N···CO<sub>2</sub> in [Pyrz – CO<sub>2</sub>] anion formed via the reaction between [Pyrz] anion and CO<sub>2</sub>, according to the previous reports. [40,69] Additionally,

an interesting result is that the amount of [CO<sub>2</sub> – EG – CO<sub>2</sub>]<sup>2-</sup> and [EG – CO<sub>2</sub>] species decreased while [Pyrz – CO<sub>2</sub>] species increased during more than 15 wt% CO<sub>2</sub> was captured. Moreover, in the <sup>13</sup>C NMR spectrum of fresh [DBNH][Pyrz]:EG (1:1), a typical signal at 161.2 ppm, assigning to the carbon of –N–C – N – in [DBNH] cation, was obviously shifted down-field to 163.8 ppm during CO<sub>2</sub> absorption, because of the interaction between [DBNH] cation and carboxylate anions. [74].

Furthermore, the comparison of <sup>13</sup>C NMR spectra of [DBNH][Pyrz]:SN (1:1) and [N<sub>2222</sub>][Pyrz]:EG (1:1) with [DBNH][Pyrz]:EG (1:1) before and after CO<sub>2</sub> absorption at 20 °C under CO<sub>2</sub> partial pressure of 0.05 bar were used to further verify the different carbonyl carbons of and O···CO<sub>2</sub> carbonate species and N···CO<sub>2</sub> carbamate species (Fig. 11). It can be seen that compared with two new shifts at 160.9 and 158.4 ppm were present in the <sup>13</sup>C NMR spectrum of [DBNH][Pyrz]:EG (1:1) + CO<sub>2</sub>, only one new shift at 160.7 ppm was present in the <sup>13</sup>C NMR spectrum of [DBNH][Pyrz]:SN (1:1) + CO<sub>2</sub>, while two new shifts at 160.4 and 157.8 ppm were present in the <sup>13</sup>C NMR spectrum of [N<sub>2222</sub>][Pyrz]:EG (1:1) + CO<sub>2</sub>. These results clearly showed that that 163 ppm as well as 159.5 ppm were both appeared while 157.5 and 157.3 ppm were both absent.

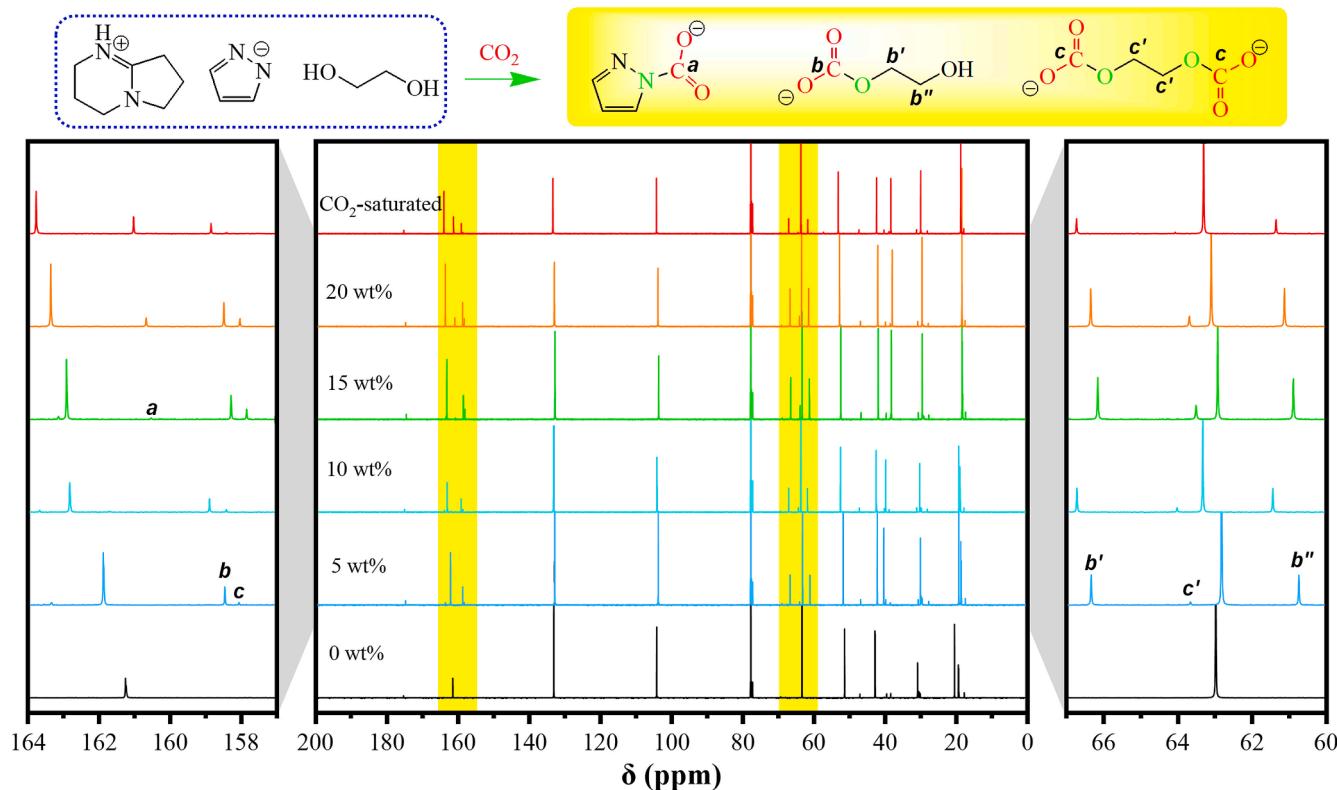
Moreover, the mechanism of CO<sub>2</sub> absorption by [DBNH][Pyrz]:EG (1:1) was further investigated by FT-IR spectroscopy (Fig. 12). It can be seen that the intensity of three new stretching vibration peaks at 1682, 1625 and 1310 cm<sup>-1</sup> increased gradually during CO<sub>2</sub> absorption. These peaks could be assigned to a stretching C=O vibration in N–CO<sub>2</sub> ( $\nu = 1682$  cm<sup>-1</sup>), two stretching C=O vibrations in O–CO<sub>2</sub> ( $\nu = 1625$  cm<sup>-1</sup>), and one stretching C–O vibration ( $\nu = 1310$  cm<sup>-1</sup>) according to the previous reports. [69,75] Although it is impossible to distinguish different C=O vibrations in [EG–CO<sub>2</sub>] and [CO<sub>2</sub>–EG–CO<sub>2</sub>]<sup>2-</sup>, it is clear that the cooperative interaction were formed during more CO<sub>2</sub> absorption. Besides, other three new peaks at 3139, 2975 and 2886 cm<sup>-1</sup> increased gradually during CO<sub>2</sub> capture. Based on the previous reports, [76,77] the first peak could be attributed to N–H stretching vibration in neutral molecule Pyrz, while other two peaks belong to COO···H hydrogen bonds. Due to the deprotonation of –OH in EG by [Pyrz] anion, the peak at 960 cm<sup>-1</sup> belong to the bending vibration of –OH decreased gradually during CO<sub>2</sub> capture. [78] Thus, these results suggested that the anion-induced multi-site cooperations of O···CO<sub>2</sub> and N···CO<sub>2</sub> were the main reason of ultrahigh CO<sub>2</sub> capacities.

Based on the observed products and previous reports, [79–81] the possible mechanism of CO<sub>2</sub> capture by [DBNH][Pyrz]:EG (1:1) could be proposed as Fig. 13. It showed that these reactions were initiated by [Pyrz] anions and resulted in two routes with three forms of absorbed CO<sub>2</sub>, including two kinds of O···CO<sub>2</sub> carbonates and a kind of N···CO<sub>2</sub> carbamate.

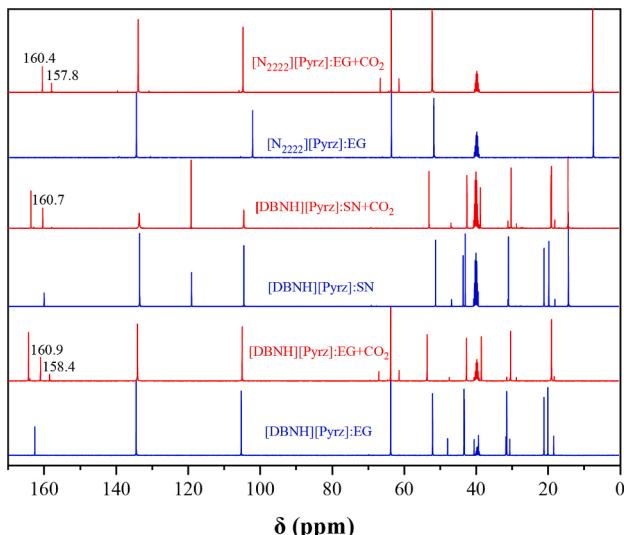
### 3.2.4. Thermodynamics analysis of CO<sub>2</sub> absorption

It is clear that the multi-site cooperations of CO<sub>2</sub> capture by [DBNH][Pyrz]:EG (1:1) simultaneously included several reactions and resulted in the difficulty in the analysis of thermodynamic properties, such as the chemical equilibrium constant ( $K$ ), the change of molar enthalpy of the reaction ( $\Delta_r H_m$ ), the change of molar entropy of the reaction ( $\Delta_r S_m$ ), and the change of molar Gibbs free energy of the reaction ( $\Delta_r G_m$ ), for each reaction. However, it is probably to estimate these properties as the apparent chemical equilibrium constant ( $K'$ , in dimensionless), the apparent change of molar enthalpy of the reaction ( $\Delta_r H'_m$ , in kJ mol<sup>-1</sup>), the apparent change of molar entropy of the reaction ( $\Delta_r S'_m$ , in J mol<sup>-1</sup> K<sup>-1</sup>), and the apparent change of molar Gibbs free energy of the reaction ( $\Delta_r G'_m$ , in kJ mol<sup>-1</sup>). [82,83] That is because of all cooperative reactions were induced by [Pyrz] anion through 1:1 equimolar chemical reaction and can be considered as [Pyrz] + CO<sub>2</sub> → [Pyrz]·CO<sub>2</sub> under low concentration CO<sub>2</sub> (particularly 500 ppm).

Here, the apparent thermodynamics analysis of CO<sub>2</sub> absorption by [DBNH][Pyrz]:EG (1:1) was investigated via testing the CO<sub>2</sub> absorption capacities at different temperatures (20, 30, 40, 50, and 60 °C) in the units of wt% and mole of CO<sub>2</sub> per mole of [Pyrz] under CO<sub>2</sub> partial pressure of 0.0005 bar. The  $K'$  could be obtained by the following



**Fig. 10.** Comparison of  $^{13}\text{C}$  NMR spectra of [DBNH][Pyrz]:EG (1:1) before and during  $\text{CO}_2$  absorption at  $20\text{ }^\circ\text{C}$  under  $\text{CO}_2$  partial pressure of 0.05 bar (solvent:  $\text{CDCl}_3$ ).

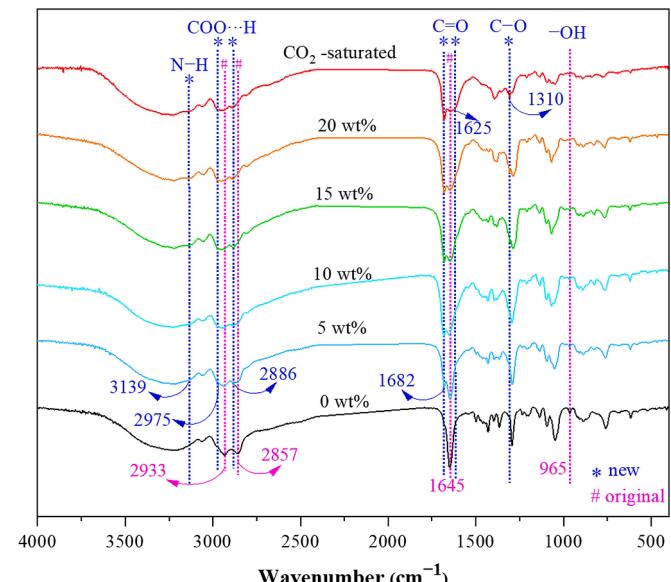


**Fig. 11.** Comparison of  $^{13}\text{C}$  NMR spectra of [DBNH][Pyrz]:EG (1:1), [DBNH][Pyrz]:SN (1:1), and [N<sub>2222</sub>][Pyrz]:EG (1:1) before and after  $\text{CO}_2$  absorption at  $20\text{ }^\circ\text{C}$  under  $\text{CO}_2$  partial pressure of 0.05 bar (solvent: d6-DMSO).

equation:

$$K' = \frac{Z_{\text{chem}}}{(1 - Z_{\text{chem}})P/P^0}$$

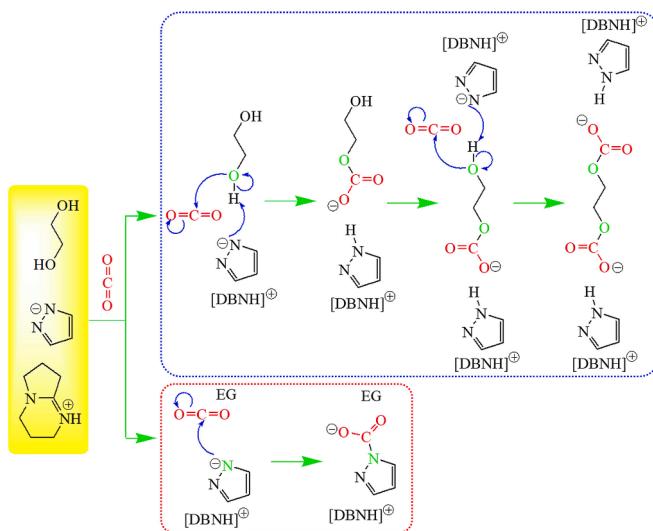
where  $Z_{\text{chem}}$  is the chemical absorption capacity in mole of  $\text{CO}_2$  per mole of [Pyrz]. The capacity at different temperatures in different units as well as the calculated values of  $K'$  and  $\ln K'$  were listed in Table 4.  $K'$  and  $\ln K'$  values decreased with the increase of temperature. For the instance,  $K'$  at 20, 30, 40, 50, and  $60\text{ }^\circ\text{C}$  were 7955, 5220, 2092, 1422, and 443.5,



**Fig. 12.** Comparison of FT-IR spectra of [DBNH][Pyrz]:EG (1:1) before and after the absorption of  $\text{CO}_2$  at  $20\text{ }^\circ\text{C}$  and 0.05 bar.

respectively, suggesting that  $\text{CO}_2$  absorption could be easily performed at low temperature. Due to the quite narrow temperature range, the thermodynamic properties of  $\Delta_rH_m$ ,  $\Delta_rS_m$ , and  $\Delta_rG_m$  could be readily obtained by the following equations from  $\ln K'$ ,  $T$  (in K), and ideal gas constant  $R$  ( $8.314\text{ J}\cdot\text{mol}^{-1}\text{ K}^{-1}$ ):

$$\ln K' = -\frac{\Delta_rH_m}{RT} + \frac{\Delta_rS_m}{R}$$



**Fig. 13.** Plausible reaction mechanism of  $\text{CO}_2$  capture by [DBNH][Pyrz]:EG (1:1). Note that all hydrogen bonds are not illustrated.

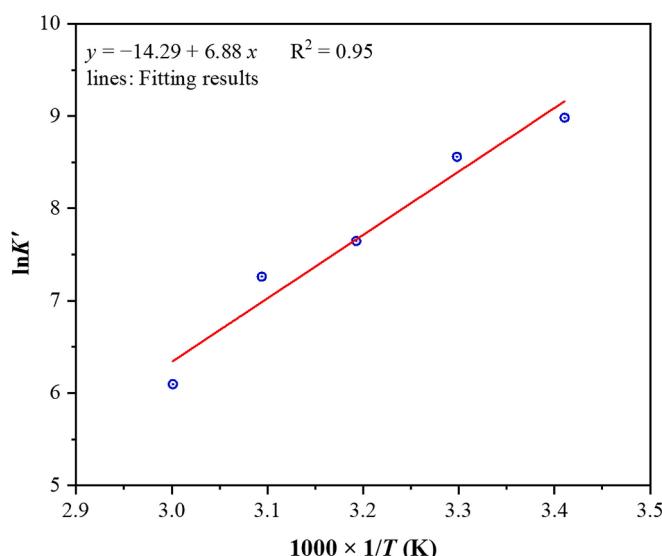
**Table 4**

Absorption capacities and thermodynamic properties for the  $\text{CO}_2$  capture by [DBNH][Pyrz]:EG (1:1) at different temperatures under  $\text{CO}_2$  partial pressure of 0.0005 bar.

T (°C)	CO <sub>2</sub> capture capacity g/g	CO <sub>2</sub> capture capacity mol CO <sub>2</sub> mol <sup>-1</sup> [Pyrz]	1/T (in 1/K)	Parameter K'	lnK'
20	0.14	0.80	3.411	7955	8.982
30	0.13	0.72	3.298	5220	8.560
40	0.09	0.51	3.193	2092	7.646
50	0.07	0.42	3.094	1422	7.260
60	0.03	0.18	3.001	443.5	6.095

$$\Delta_r G'_m = \Delta_r H'_m - T \Delta_r S'_m$$

The relationship between  $\ln K'$  and  $1/T$  was illustrated in Fig. 14, while Table 5 listed the calculated values of  $\Delta_r H'_m$ ,  $\Delta_r S'_m$ , and  $\Delta_r G'_m$ . The results showed that the values of  $\Delta_r H'_m$  and  $\Delta_r G'_m$  were negative, indicating a spontaneous and exothermic process of  $\text{CO}_2$  absorption by DES. Besides, the value of  $|\Delta_r H'_m|$  was higher than 50 kJ mol<sup>-1</sup>, indicating that the interactions between DES and  $\text{CO}_2$  were chemically.



**Fig. 14.** Slope of the linear relationship between  $\ln K'$  and  $1/T$ .

**Table 5**

Thermodynamic properties for the  $\text{CO}_2$  capture by [DBNH][Pyrz]:EG (1:1) at different temperatures under  $\text{CO}_2$  partial pressure of 0.0005 bar.

Thermodynamic property	T (°C)				
	20	30	40	50	60
$\Delta_r H'_m$ (kJ mol <sup>-1</sup> )	-57.16				
$10^3 \Delta_r S'_m$ (kJ mol <sup>-1</sup> K <sup>-1</sup> )	-118.8				
$\Delta_r G'_m$ (kJ mol <sup>-1</sup> )	-22.33	-21.14	-19.95	-18.76	-17.58

Additionally, the value of  $\Delta_r S'_m$  was also negative, suggesting that the disorder degree became smaller after  $\text{CO}_2$  absorption, another result of strong chemical interaction. Generally, because of  $\Delta_r H'_m < 0$  and  $\Delta_r S'_m < 0$  as well as  $|\Delta_r H'_m| > |\Delta_r S'_m|$ , the sign of the value of  $\Delta_r G'_m$  was determined by that of  $\Delta_r H'_m$ . Therefore,  $\Delta_r H'_m$  is more favorable than other thermodynamic properties for  $\text{CO}_2$  capture under low concentration  $\text{CO}_2$  through chemical absorption.

#### 4. Conclusions

In summary, a series of functional DESs forming from azolate ionic liquids as HBAs and EG or SN as HBDs were developed for  $\text{CO}_2$  capture. Density and viscosity as well as flow activation energies of these functional DESs were calculated. The performances of  $\text{CO}_2$  capture were tested under different temperatures and  $\text{CO}_2$  partial pressures (500 ppm–5 vol%). The results showed that, compared with different structures of these azolate-based DESs, the  $\text{CO}_2$  capacity increased linearly with the increase of pKa of azoles, and the highest  $\text{CO}_2$  capacity could be achieved by [DBNH][Pyrz]:EG (1:1). Compared with other DESs and ILs, the extremely high  $\text{CO}_2$  capture capacities of 14 wt% (3.18 mmol g<sup>-1</sup>), 25 wt% (5.68 mmol g<sup>-1</sup>), and 26 wt% (5.91 mmol g<sup>-1</sup>) could be reached under open air / 500 ppm, 2 vol%, and 5 vol%  $\text{CO}_2$ , respectively. To the best of our knowledge, these are the highest capacities for  $\text{CO}_2$  absorption by DESs and ILs under low concentrations of  $\text{CO}_2$ , *via* tuning the structures of AILs and the molar ratio of AIL to HBD. The spectroscopic investigations revealed that the anion-induced multi-site cooperations of O··· $\text{CO}_2$  and N··· $\text{CO}_2$  were the reason of ultrahigh  $\text{CO}_2$  capacities. The possible mechanism of  $\text{CO}_2$  capture by [DBNH][Pyrz]:EG (1:1) indicated that these reactions were initiated by [Pyrz] anions and resulted in two routes with three forms of absorbed  $\text{CO}_2$ , including two kinds of O··· $\text{CO}_2$  carbonates ([EG –  $\text{CO}_2$ ] and [ $\text{CO}_2$  – EG –  $\text{CO}_2$ ]<sup>2-</sup>) and a kind of N··· $\text{CO}_2$  carbamate ([Pyrz –  $\text{CO}_2$ ]). Thermodynamic properties of  $\text{CO}_2$  capture by [DBNH][Pyrz]:EG (1:1), such as the apparent chemical equilibrium constant ( $K'$ ), the apparent change of molar Gibbs free energy of the reaction ( $\Delta_r G'_m$ ), the apparent change of molar enthalpy of the reaction ( $\Delta_r H'_m$ ), and the apparent change of molar entropy of the reaction ( $\Delta_r S'_m$ ), were studied. The results indicated that  $\Delta_r H'_m$  is more favorable than other thermodynamic properties for  $\text{CO}_2$  capture under low concentration  $\text{CO}_2$  through chemical absorption. We believe that the significant improvements made in this work on  $\text{CO}_2$  capture over conventional sorbents provide an alternative strategy for industrial gas capture and utilization *via* anion-induced multi-site cooperations.

#### CRediT authorship contribution statement

**Guokai Cui:** Writing – review & editing, Writing – original draft, Supervision, Project administration, Investigation, Funding acquisition, Formal analysis, Conceptualization. **Yepin Cheng:** Visualization, Investigation, Data curation. **Wei Zhang:** Formal analysis. **Xiangyu Shen:** Validation, Formal analysis. **Lai Li:** Data curation. **Ruina Zhang:** Visualization, Methodology, Data curation. **Yaoji Chen:** Formal analysis. **Quanli Ke:** Funding acquisition, Formal analysis. **Chunliang Ge:** Formal analysis. **Huayan Liu:** Methodology, Formal analysis. **Wenyang Fan:** Resources, Formal analysis. **Hanfeng Lu:** Writing – review & editing, Supervision, Resources, Project administration, Funding acquisition, Formal analysis, Conceptualization.

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.cej.2024.159193>.

## Data availability

Data will be made available on request.

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